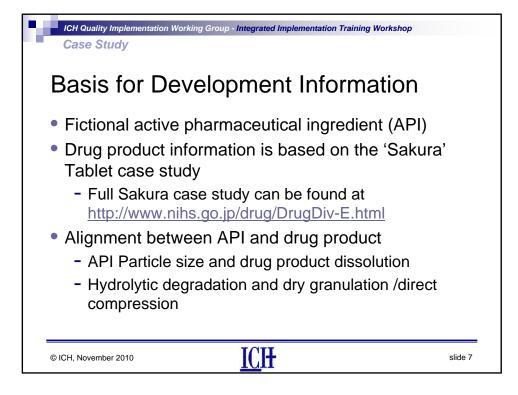
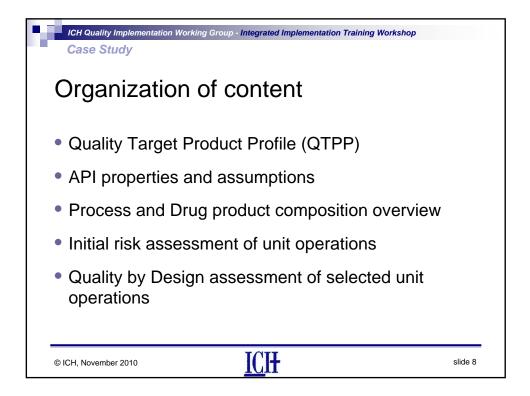
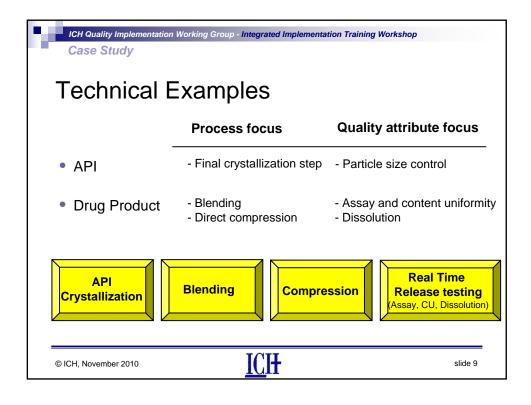
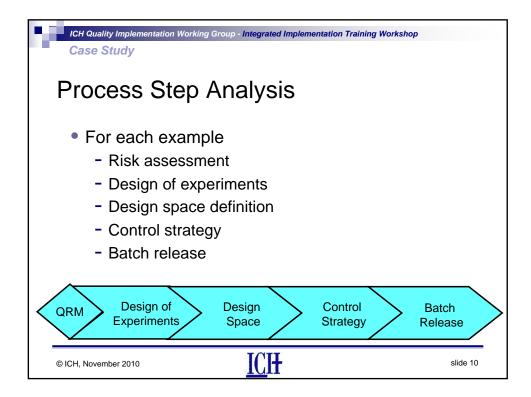


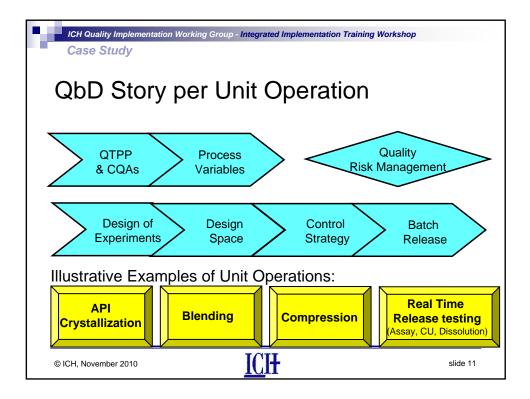
ICH Quality Implementation Working Group - Integrated Implementation Training Workshop Case Study
Purpose of Case Study
This case study is provided as an example to help illustrate the concepts and integrated implementation of approaches described in ICH Q8, Q9 and Q10. It is not intended to be the complete information on development and the manufacturing process for a product that would be presented in a regulatory filing, but focuses mainly on Quality by Design aspects to facilitate training and discussion for the purposes of this workshop.
<b>Note:</b> this example is not intended to represent the preferred or required approach
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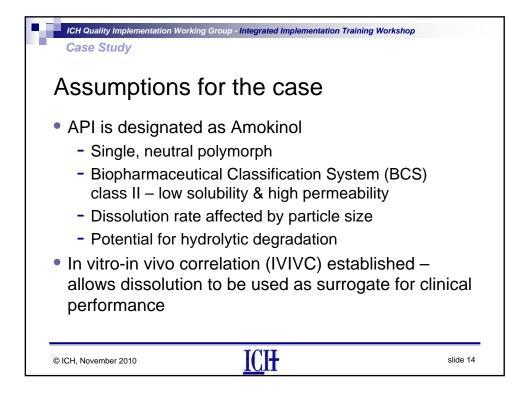


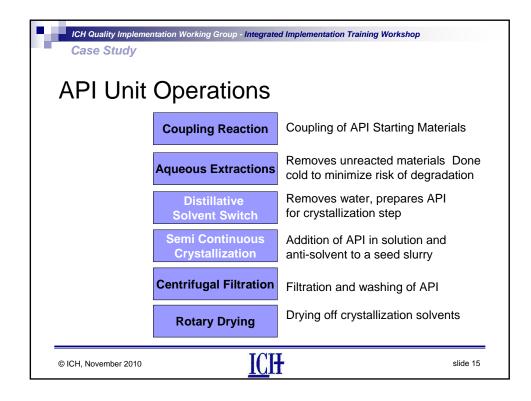




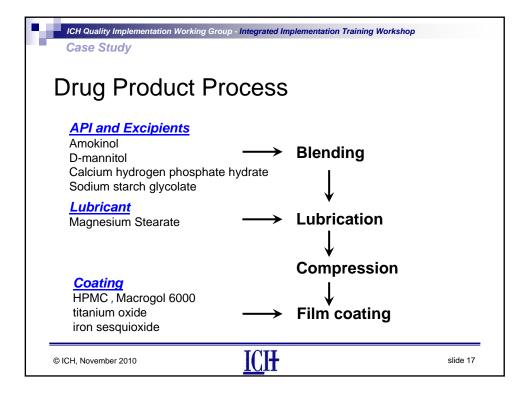
Case Study Case Study Quality Target P defines the objectives for	
Dosage form and strength	Immediate release tablet taken orally containing 30 mg of active ingredient
Specifications to assure safety and efficacy during shelf-life	Assay, Uniformity of Dosage Unit (content uniformity) and dissolution
Description and hardness	Robust tablet able to withstand transport and handling
Appearance	Film-coated tablet with a suitable size to aid patient acceptability and compliance Total tablet weight containing 30 mg of active ingredient is 100 mg with a diameter of 6 mm
product that ideally will be	hary of the quality characteristics of a drug achieved to ensure the desired quality, tak cacy of the drug product. (ICH Q8 (R2))

Case Study Quality Target F Safety and Efficacy R	Product Profile (QTF	PP)
Tablet	Characteristics / Requirements	Translation into Quality Target Product Profile (QTPP)
Dose	30 mg	Identity, Assay and Uniformity
Subjective Properties	No off-taste, uniform color, and suitable for global market	Appearance, elegance, size, unit integrity and other characteristics
Patient Safety – chemical purity	Impurities and/or degradates below ICH or to be qualified	Acceptable hydrolysis degradate levels at release, appropriate manufacturing environment controls
Patient efficacy – Particle Size Distribution (PSD)	PSD that does not impact bioperformance or pharm processing	Acceptable API PSD Dissolution
Chemical and Drug Product Stability: 2 year shelf life (worldwide = 30°C)	Degradates below ICH or to be qualified and no changes in bioperformance over expiry period	Hydrolysis degradation & dissolution changes controlled by packaging
	e – during development and commercial ma are identified, new technical information is	
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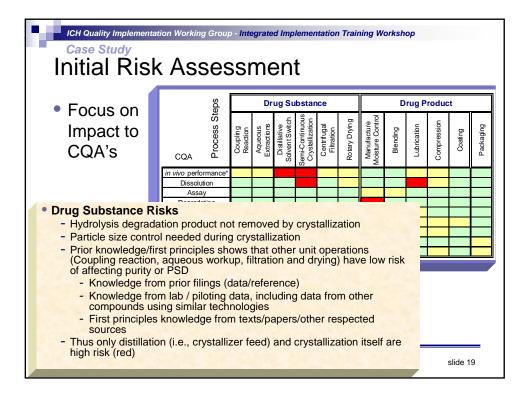


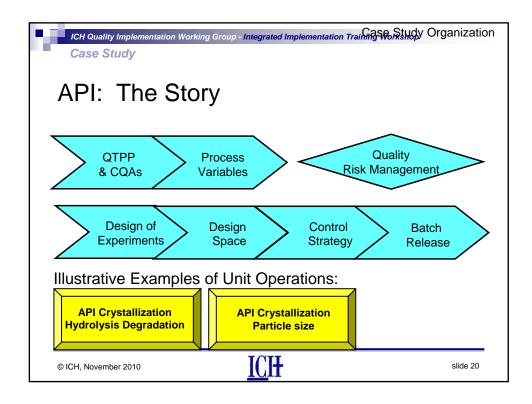


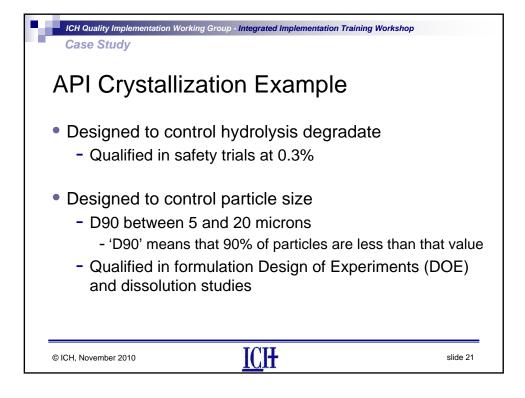
ICH Quality Implementation Working Group - Integrated Implementation Training Workshop Case Study								
Tablet	Tablet Formulation							
2.3.P.1 Description and Composition of the Drug Product (Sakura Tablet, Film-coated Tablet)								
Function	Specification	Excipient	Sakura Tablet 30 mg					
Active ingredient	Separate specification	Amokinol	30 mg / tablet (100 mg)					
Excipient		Calcium hydrogen phosphate hydrate	Appropriate amount					
Excipient		D-mannitol	10 mg					
Disintegrant	Pharmacopoeial	Sodium starch glycolate	5  mg					
Lubricant	or other	Magnesium stearate	2 mg					
Coating agent	compendial	HPMC	2.4 mg					
Polishing agent	specification	Macrogol 6000	0.3 mg					
Coloring agent		Titanium oxide	0.3 mg					
Coloring agent		Iron sesquioxide	Trace amount					
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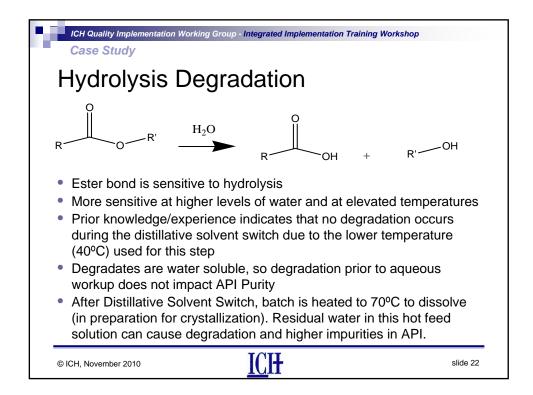


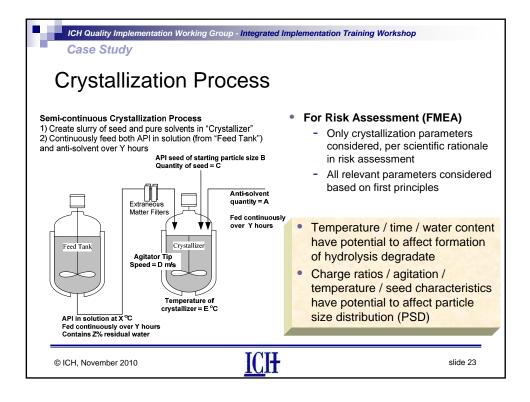
Case Study	Overall Risk Assessment for Process											
no impact to CQA     known or potential impact to CQA     current controls mitigate risk		Process Steps										
<ul> <li>known or potential impact to CQA</li> <li>additional study required</li> </ul>		Dr	ug Su	ıbstar	nce			D	rug P	roduc	t	
* includes bioperformace of API and so (API purity)	Coupling Reaction	Aqueous Extractions	Distillative Solvent Switch	Semi-Continuous Crystallization	Centrif ugal Filtration	Rotary Drying	Manufacture Moisture Control	Blending	Lubrication	Compression	Coating	Packaging
<i>in vivo</i> performance* Dissolution Assay												
Degradation Content Uniformity Appearance Friability												
Stability-chemical Stability-physical												
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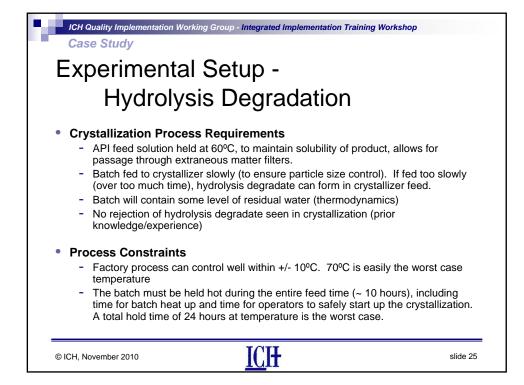


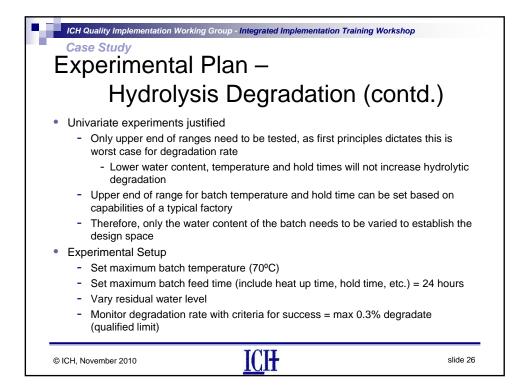


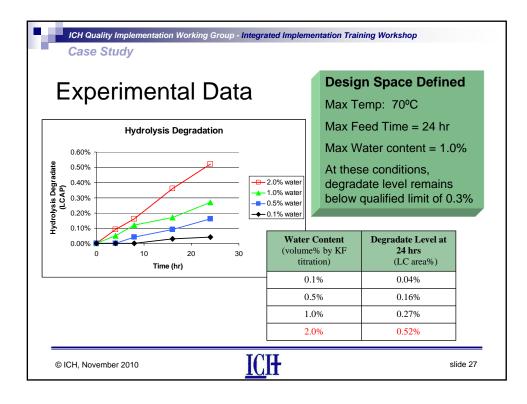


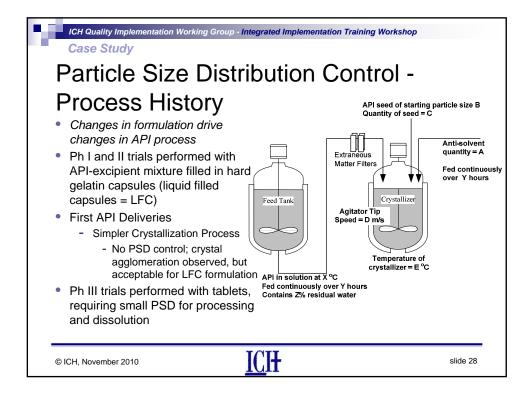


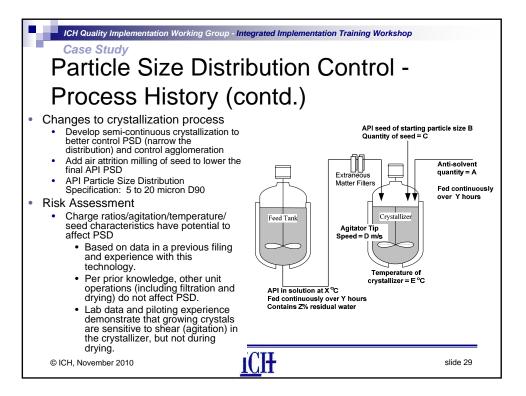
Dick A	accomment (		'N	Л		A): Durity Control
						A): Purity Control
	will have on purity? 1) minimal t variations in will occur? 1) u					
What is our Ability to Detec	t a meaningful variation in	ata	a m	iea	ningful	control point? 1) certain 5) moderate 9) unlikely
Unit Operation	Parameter	1112	15/00		1 a) RPN	Comments
Distillative Solvent Switch	Temperature / Time, etc.	1	5	1	5	Distillation performed under vacuum, at low temperature, minimizing risk of hydrolysis
Distillative Solvent Switch / Crystallization	Water content at end of Distillation (Crystallization Feed)	9	5	1	45	Higher water = higher degradation In process control assay should ensure detection and
Crystallization API Feed Solution	Feed Temperature	9	5	1	45	Higher temperature = higher degradation Temperature alarms should enable quick detection and control
Crystallization API Feed Solution	Addition Time	9	1	5	45	Longer time = higher degradation Detection of prolonged addition time may occur too late to prevent some degradation
Crystallization	Seed wt percentage	1	1	1	1	This parameters cannot impact impurity rejection, since no rejection of hydrolysis degradate occurs.
Crystallization	Antisolvent percentage (charge ratio)	1	1	1	1	This parameters cannot impact impurity rejection, since no rejection of hydrolysis degradate occurs.
Crystallization	Crystallization temperature	1	5	1	5	Temperature is low enough that no degradation will occur.
Crystallization	Other crystallization parameters	1	1	1	1	These parameters cannot impact impurity rejection, since no rejection of hydrolysis degradate occurs.







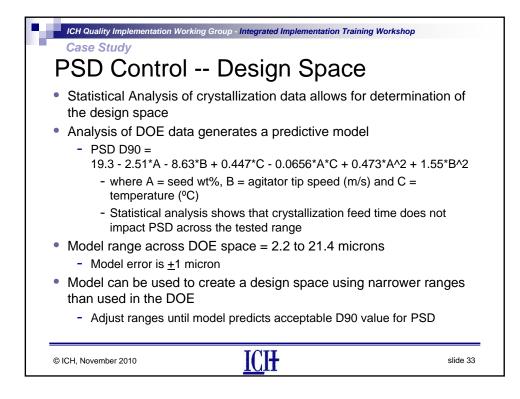


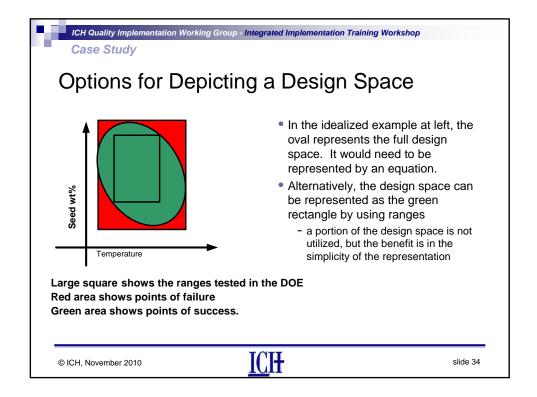


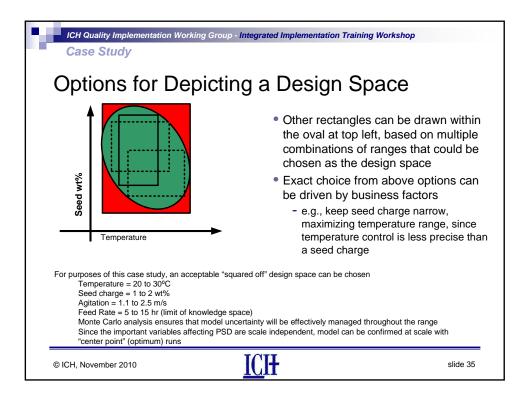
ICH Quality Implementation Working Group - Integrated Implementation Training Workshop Case Study Risk Assessment: Particle Size Distribution (PSD) Control								
will have on PSD? 1) minimation	nal 5) n	nod	lerat	te 9) s	significant			
Parameter	Im	2 0 0 0 0	0.00	RPN	Comments			
Feed Temperature	1	5	1	5	Prior knowledge (slowness of crystallization kinetics) ensures that the hot crystallizer feed will be well dispersed and thermally equilibrated before crystallizing. Hence no impact of feed temp variation on crystal size.			
Water content of Feed	1	5	5	25	Prior knowledge (solubility data) shows that small variations in water do not affect crystalliation kinetics.			
Addition Time (Feed Rate)	9	5	9	405	Fast addition could result in uncontrolled crystallization. Detection of short addition time could occur too late to prevent this uncontrolled crystallization, and thus impact final PSD.			
Seed wt percentage	9	5	5	225	Prior knowledge (Chemical Engineering theory) highlights seed wt percentage variations as a potential source of final PSD variation			
Antisolvent percentage	1	1	1	1	Yield loss to crystallization already low (< 5%), so reasonable variations in antisolvent percentage (+/- 10%) will not affect the percent of batch crystallized, and will not affect PSD			
Temperature	9	5	9	405	Change in crystallization temperature is easily detected, but rated high since no possible corrective action (such as, if seed has been dissolved)			
Agitation (tip speed)	9	5	5	225	Prior knowledge indicates that final PSD highly sensitive to agitation during crystallization, thus requiring further study.			
Seed particle size distribution	9	1	1	9	Seed PSD controlled by release assay performed after air attrition milling.			
Feed Concentration	1	1	1	1	Same logic as for antisolvent percentage			
	y SSESSMET Size Distribut Size Distribut Size Distribut Size Distribut Size Distribut Parameter Feed Temperature Water content of Feed Addition Time (Feed Rate) Seed wt percentage Antisolvent percentage Temperature Agitation (tip speed) Seed particle size distribution	Y         SSEESSMENT:         Size Distributio         Size Distributio         Yariations in	Y         SSEESSMEAL:         Size Distribution         Size Distribution         Size Distribution         Second Distribution         Parameter         Parameter         Feed Temperature         Read Temperature         Addition Time (Feed Rate)         Seed wt percentage         Antisolvent percentage         Agitation (tip speed)         Seed particle size distribution	Y         SSESSMENT:         Size Distribution         Size Distribution         Size Distribution         Second Stribution         Will have on PSD? 1) minimal 5) modera         variations in at a meaningful variation in	Y         SSESSMENT:         Size Distribution (P         Variations in at a meaning         Parameter       Size (P         Parameter       Size (P         Vater content of Feed       1       5       1       5         Addition Time (Feed Rate)       9       5       9       405         Seed wt percentage       1       1       1       1         Temperature       9       5       9       405         Agitation (tip speed)       9       5       5       225         Seed particle size distribution       9       1       1			

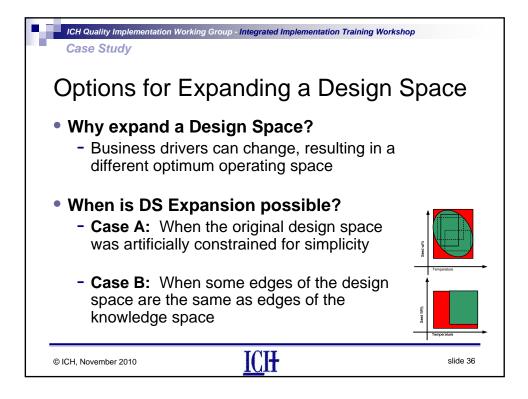
	sessmen Size Distribut		h	(D	SD) Control
What is the <b>Impact</b> that		nal 🕤 n	nod	erate 9	) significant
	nat variations in will occur? ect a meaningful variation in				nderately likely 9) highly likely aful control point? 1) certain 5) moderate 9) unlikely
Unit Operation	Parameter	ineast.	104	RPN	Comments
Crystallization	Feed Temperature	1 5	1	5	Prior knowledge (slowness of cryst the hot crystallizer feed will be well equilibrated before crystallizing. H variation on crystal size.
Crystallization	Water content of Feed	1 5	5	25	Prior knowledge (solubility data) shows that small variations in water do not affect crystalliation kinetics.
Crystallization	Addition Time (Feed Rate)	9 5	9	405	Fast addition could result in uncontrolled crystallization. Detection of short addition time could occur too late to prevent this uncontrolled crystallization, and thus impact final PSD.
Crystallization	Seed wt percentage	9 5	5	225	Prior knowledge (Chemical Engineering theory) highlights seed wt percentage variations as a potential source of final PSD variation
Crystallization	Antisolvent percentage	1 1	1	1	Yield loss to crystallization already low (< 5%), so reasonable variations in antisolvent percentage (+/- 10%) will not affect the percent of batch crystallized, and will not affect PSD
Crystallization	Temperature	9 5	9	405	Change in crystallization temperature is easily detected, but rated high since no possible corrective action (such as, if seed has been dissolved)
Crystallization	Agitation (tip speed)	9 5	5	225	Prior knowledge indicates that final PSD highly sensitive to agitation during crystallization, thus requiring further study.
Crystallization	Seed particle size distribution	9 1	1	9	Seed PSD controlled by release assay performed after air attrition
Crystallization	Feed Concentration	4 4	1	- 1	milling. Same logic as for antisolvent percentage

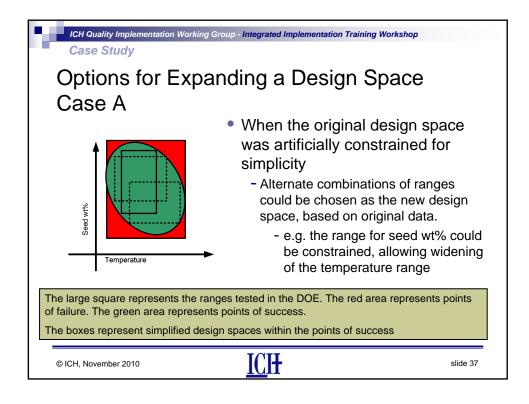
ICH Quality Implementation Working Group - Integrate Case Study					
Experimental Design	i, PS		CC Factors		Response
	Feed Rate (hrs)	Seed (wt%)	Temp °C	Tip Speed m/s	D90 (microns)
agitation tip speed crystallization temperature	15 5	1 5	10 10	0.44 0.44	13.5 14.5
<ul> <li>Experimental ranges based on QTPP and chosen by:</li> </ul>	5 15 5	1 5 1	10 10 30	2.67 2.67 0.44	5.5 2.2 21.4
<ul> <li>Prior knowledge: estimates of what ranges would be successful</li> </ul>	15 15 5	5 1 5	30 30 30	0.44 2.67 2.67	13.5 12.4 7.4
<ul> <li>Operational flexibility: ensure that ranges are suitable for factory control strategy</li> </ul>		3 3 3	20 20 20	1.56 1.56 1.56	7.8 8.3 6.1
•Experimental Results: D90 minimum - Extremes are outside of the desired					
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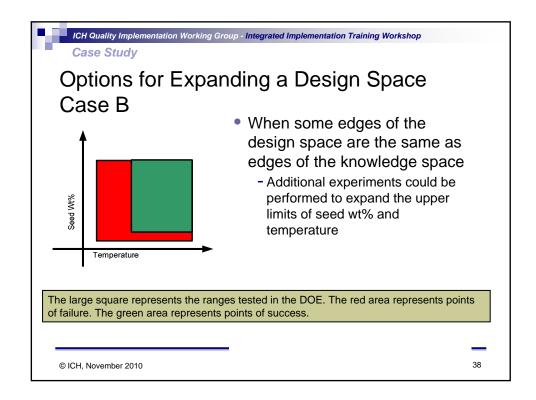


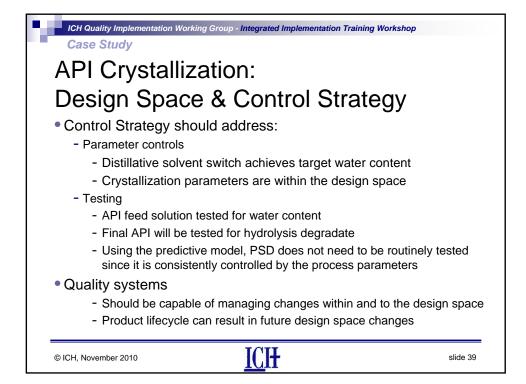




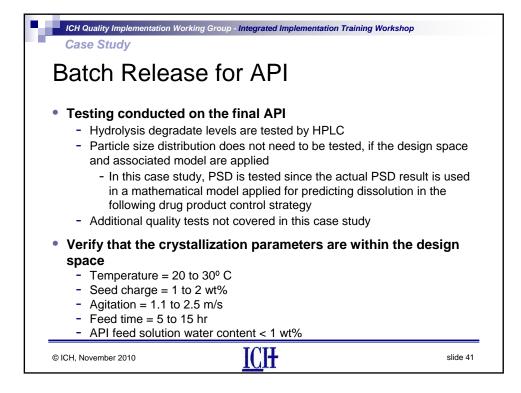


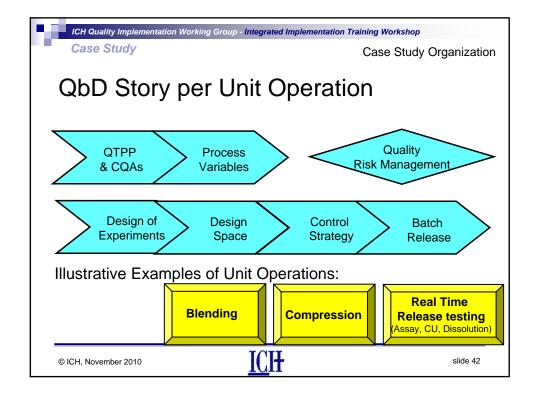


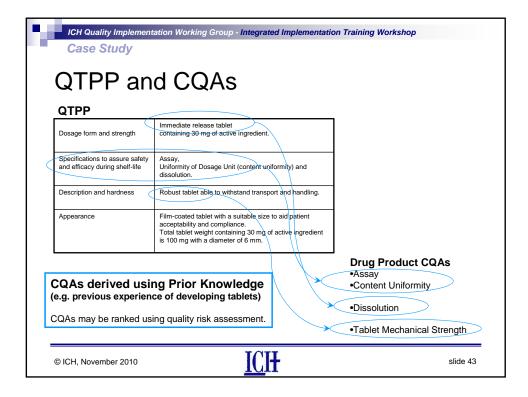


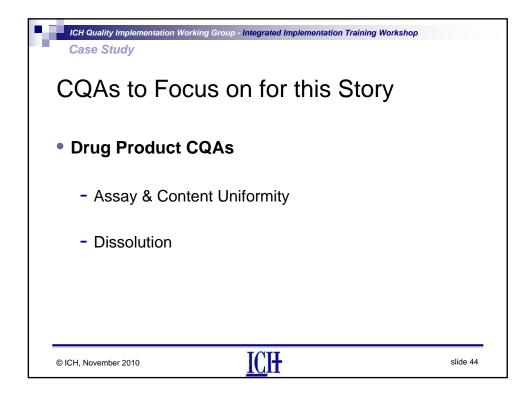


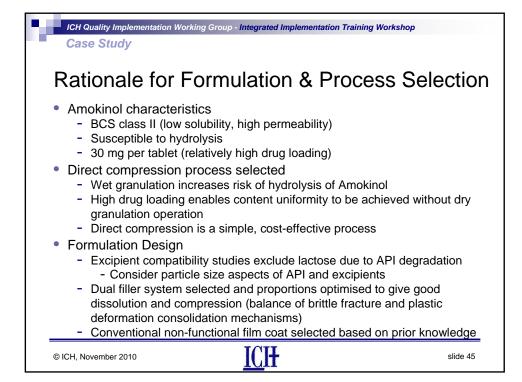
Case S API (	<sub>Study</sub> Crystalli	zation:		tion Training Workshop
Particle Size	Crystallization	Temperature	20 to 30°C	Control between 23 and 27°C
Particle Size	Crystallization	Feed Time	5 to 15 hours	Control via flow rate settings
Particle Size	Crystallization	Agitation	1.1 to 2.5 m/s	Quality system should ensure changes in agitator size result in change to speed setting
Particle Size	Crystallization	Seed Wt%	1 to 2 wt%	Controlled through weigh scales and overcheck
Hydrolysis Degradate	Distillation / Crystallization	Water Content	< 1 wt%	Control via in process assay
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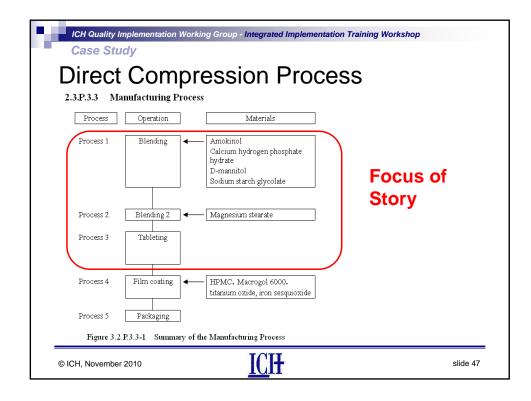


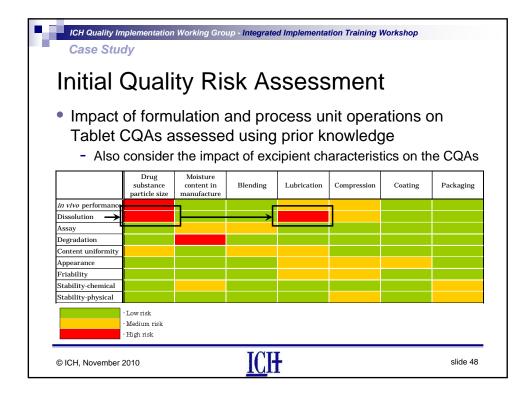


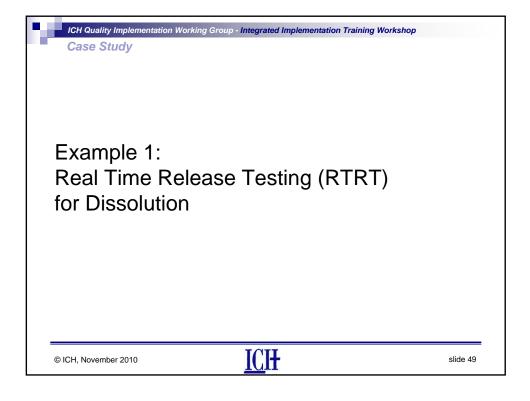


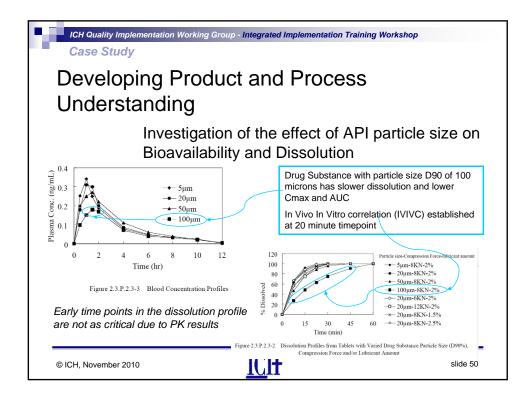


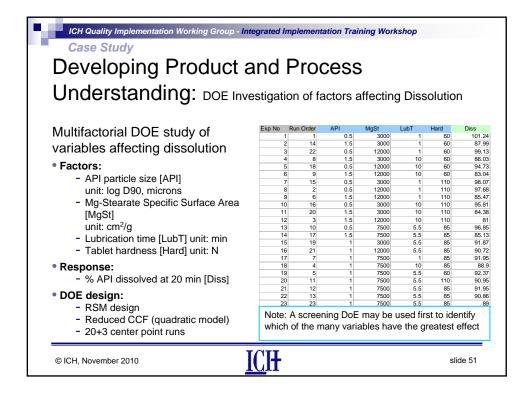
ICH Quality Im	Ű	p - Integrated Implementation Training Wor	kshop					
Tablet	Tablet Formulation							
	2.3.P.1 Description and Composition of the Drug Product (Sakura Tablet, Film-coated Tablet)							
Function	Specification	Excipient	Sakura Tablet 30 mg					
Active ingredient	Separate specification	Amokinol	30 mg / tablet (100 mg)					
Excipient		Calcium hydrogen phosphate hydrate	Appropriate amount					
Excipient	Pharmacopoeial or other compendial	D-mannitol	10 mg					
Disintegrant	specification.	Sodium starch glycolate	5 mg					
Lubricant	May have additional —	Magnesium stearate	2 mg					
Coating agent	requirements for	HPMC	2.4 mg					
Polishing agent	Functionality Related	Macrogol 6000	0.3 mg					
Coloring agent	Characteristics	Titanium oxide	0.3 mg					
Coloring agent		Iron sesquioxide	Trace amount					
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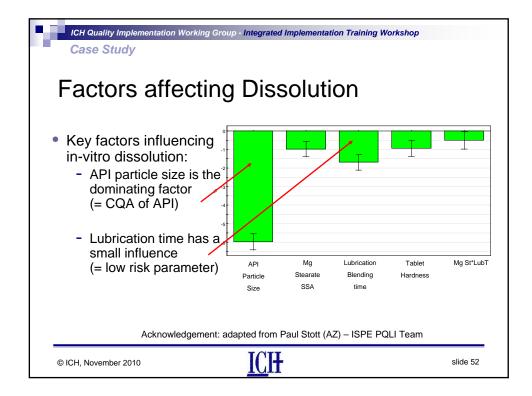


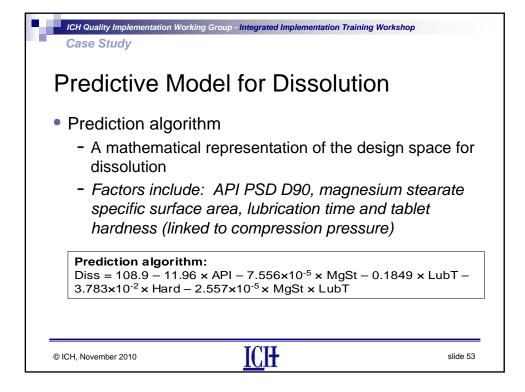




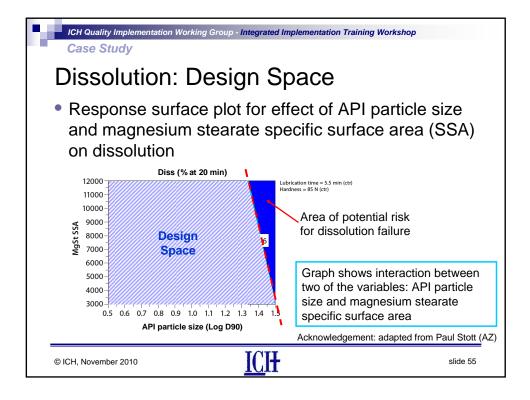


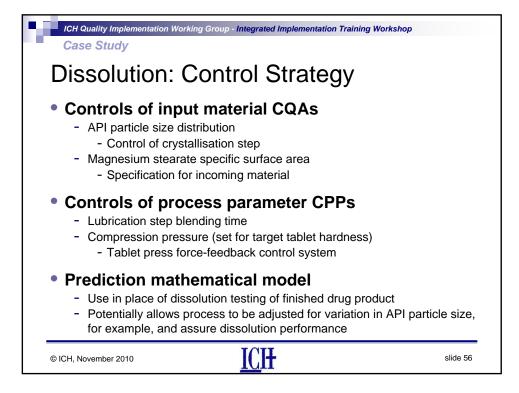


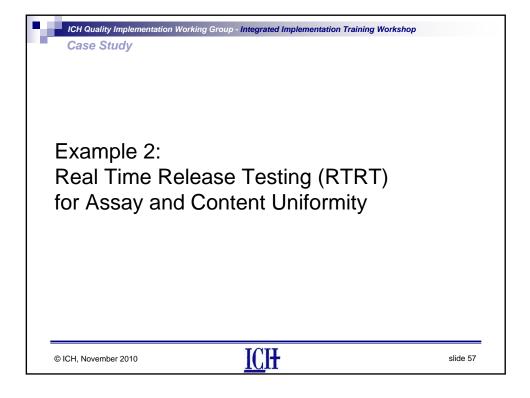


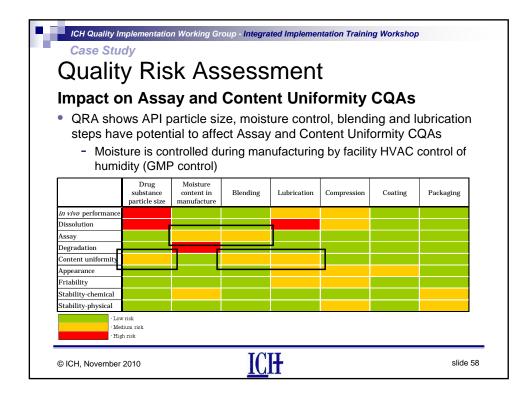


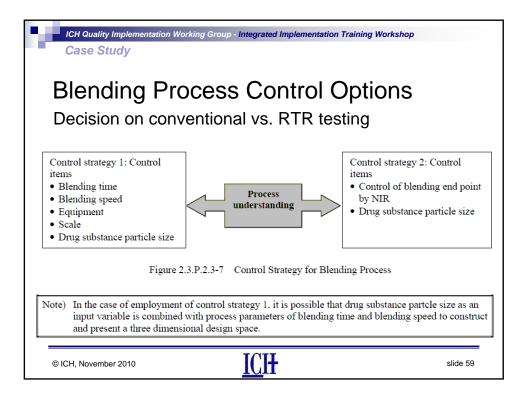
ICH Quality Implementation W Case Study	/orking Group - <b>Integrat</b>	ed Implementation Training	Workshop						
Predictive M	Predictive Model for Dissolution								
<ul> <li>Confirmation of</li> <li>compare mode</li> </ul>	riability (predi model I results vs. act I verification wit	ctability, measur ual dissolution res h dissolution testir	ults for batches						
	Batch 1	Batch 2	Batch 3						
Model prediction	89.8	87.3	88.5						
Dissolution testing result	5								
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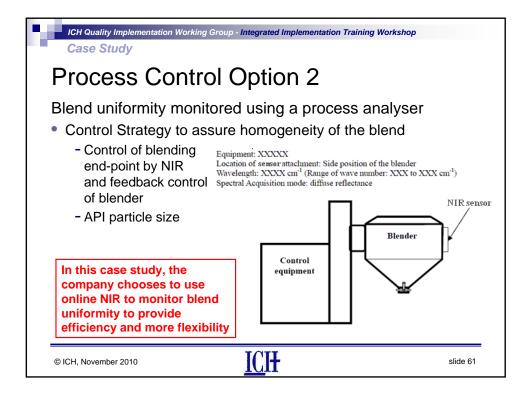


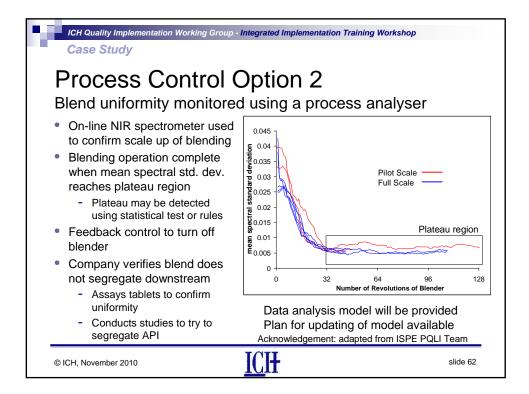


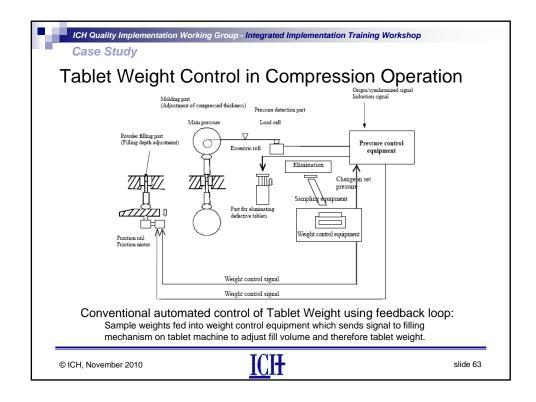


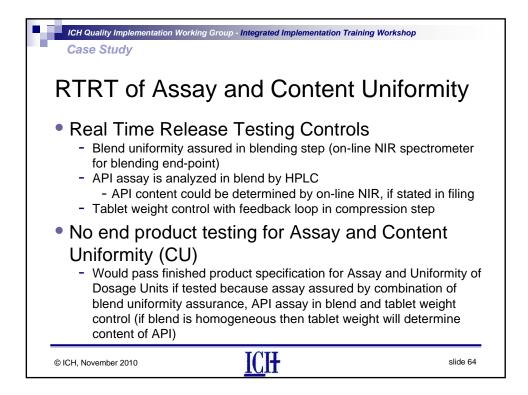


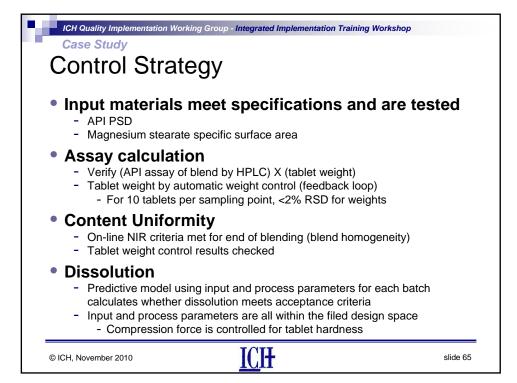
Cas	e Study			ng Group - Integ	nated Implement	tation Training V	Vorkshop	
dev	<b>velop a</b> Factors	l <b>De</b> Inve	sign S stigated	Space	ess Paran Blending tim		sessment	to
	Experiment No.	Run	Condition	Blending time (minutes)	Rotation speed (rpm)	Blender	Particle size D90 (µm)	
	1	2	varied	2	10	V type	5	x
	2	7	varied	16	10	V type	40	
2	3	10	varied	2	30	V type	40	
<u>.</u>	4	5	varied	16	30	V type	5	
ŝ	5	6	varied	2	10	Drum type	40	
design	6	1	varied	16	10	Drum type	5	
	7	8	varied	2	30	Drum type	5	
DOE	8	11	varied	16	30	Drum type	40	
Ď	9	3	standard	9	20	V type	20	
	10	12	standard	9	20	Drum type	20	
	11	9	standard	9	20	V type	20	

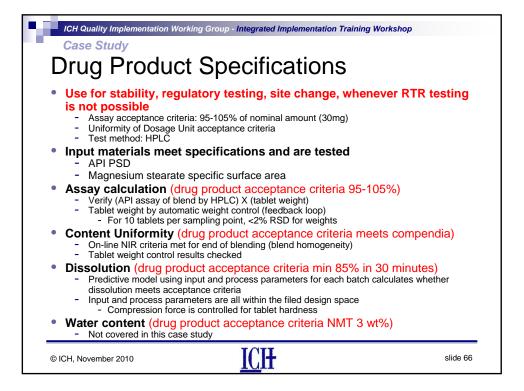


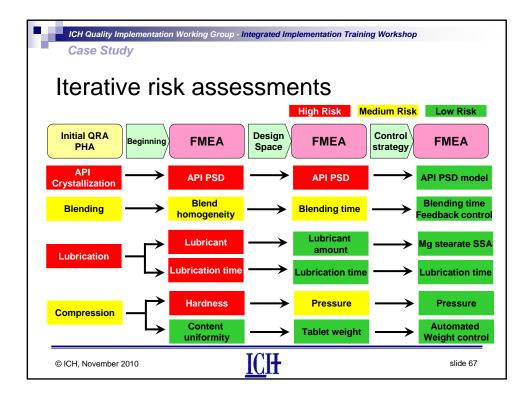


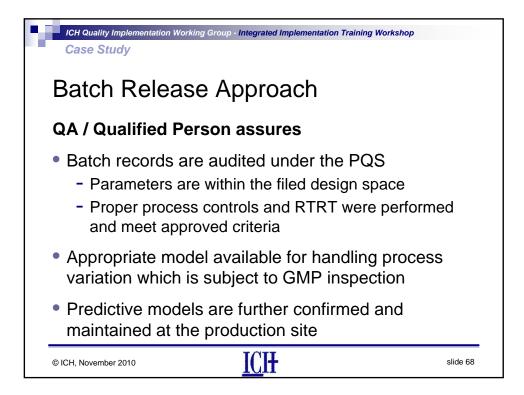


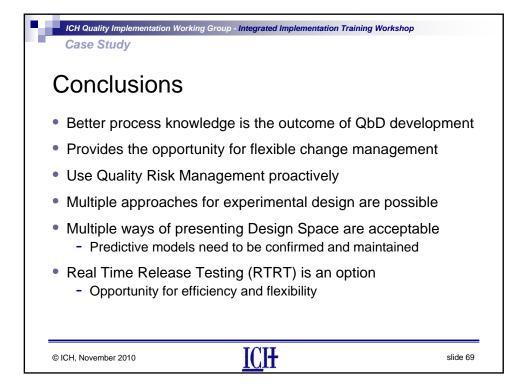


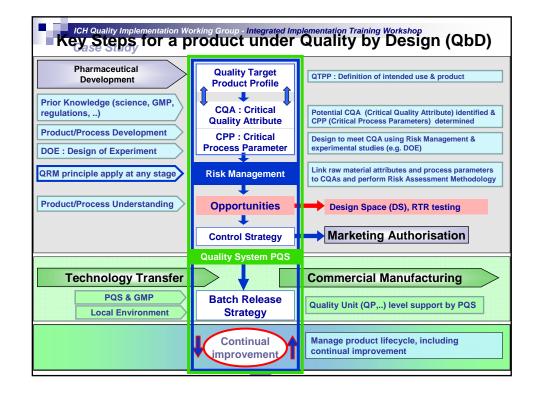


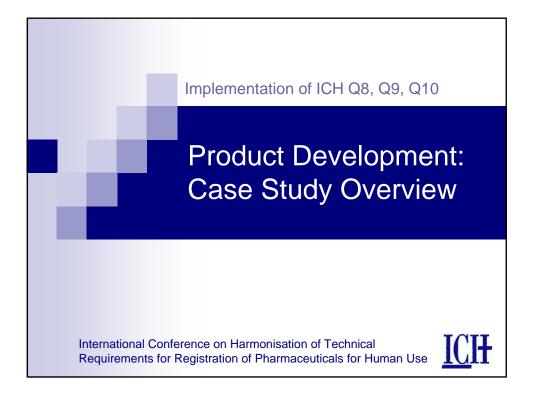


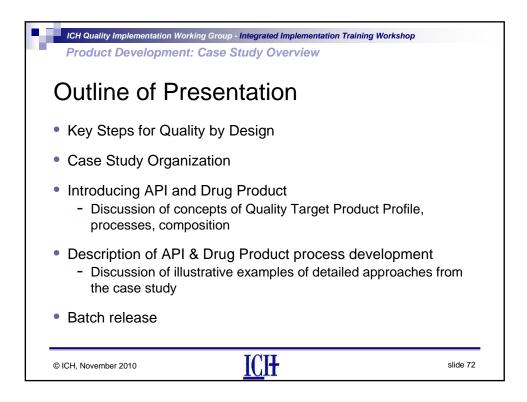


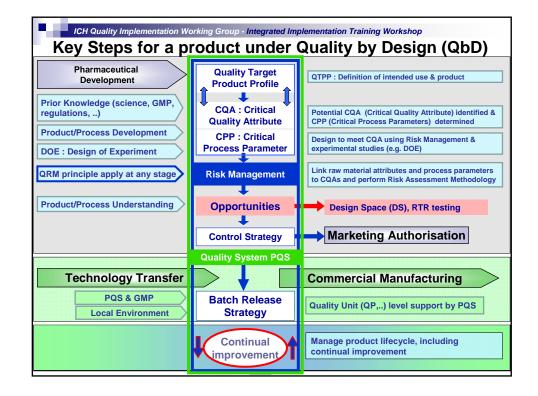


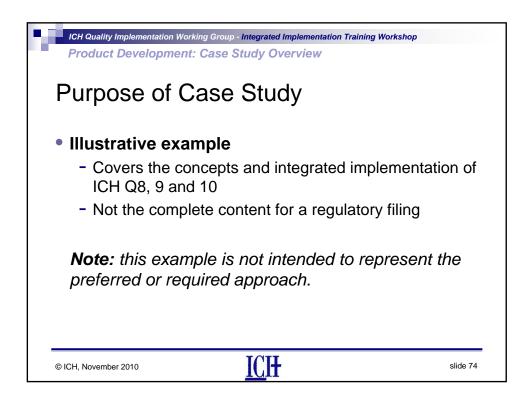


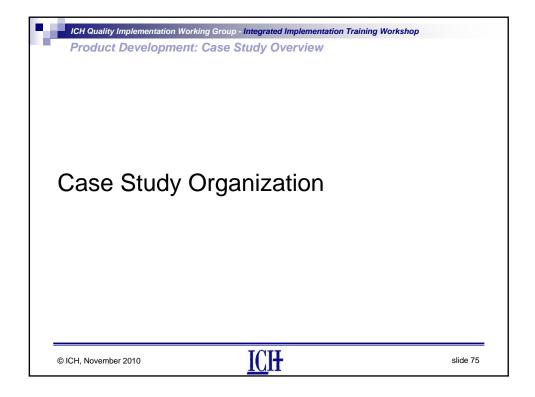


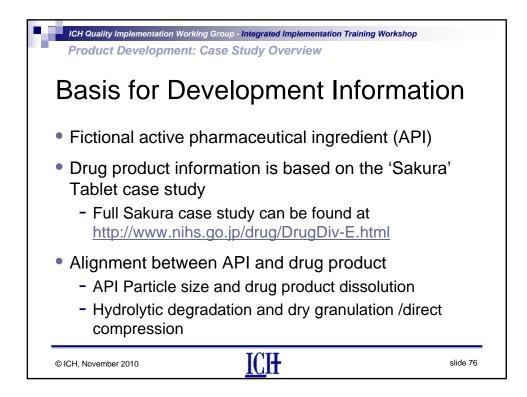




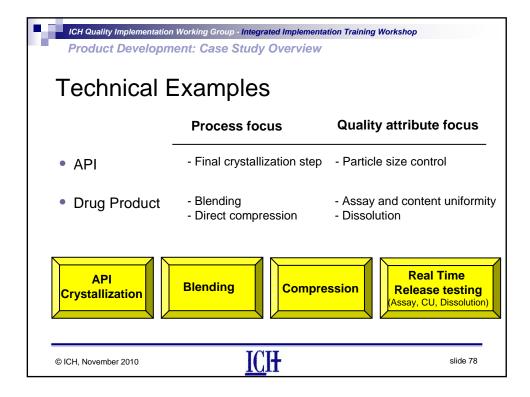


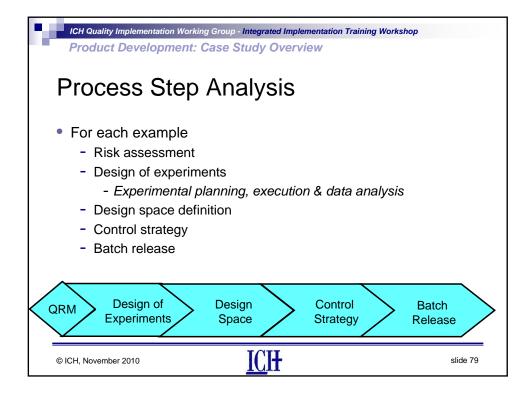


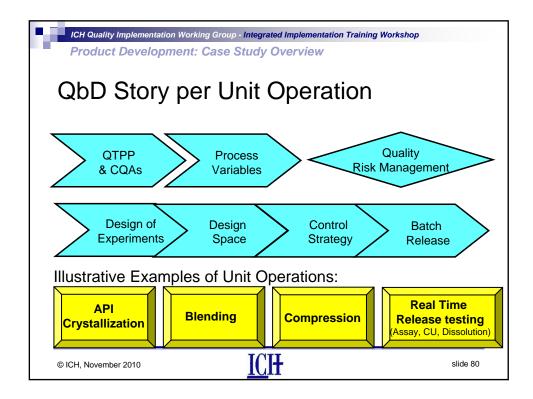


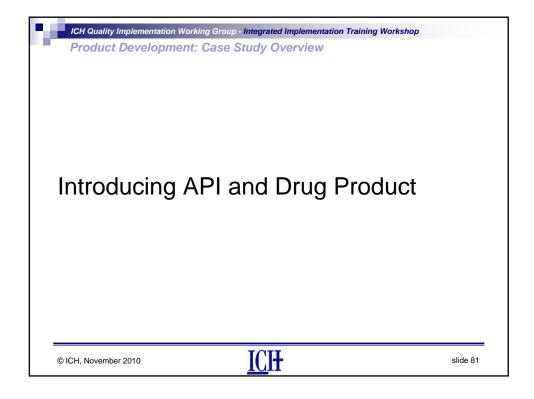


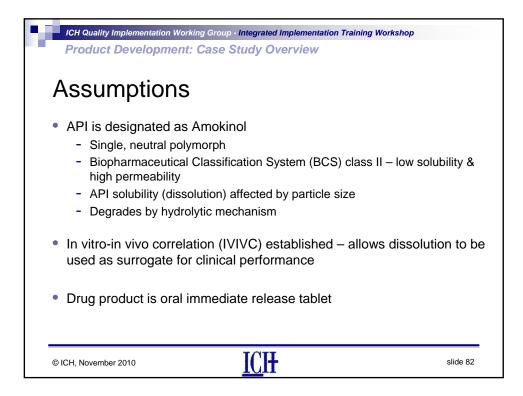


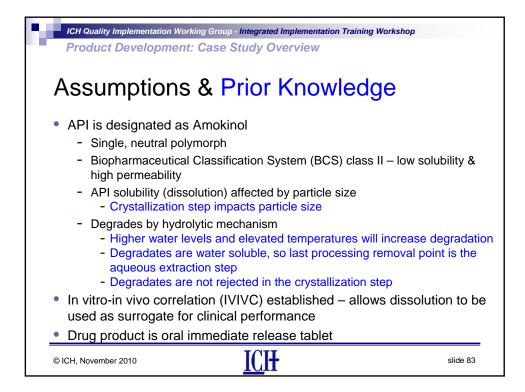




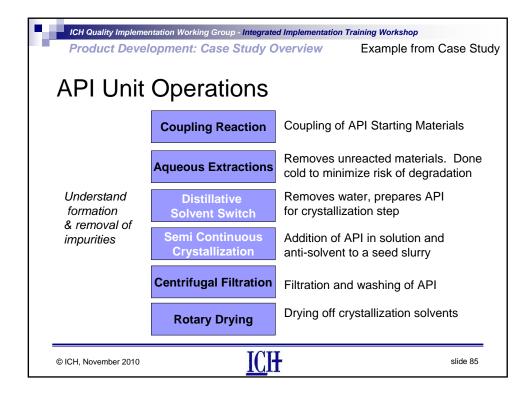




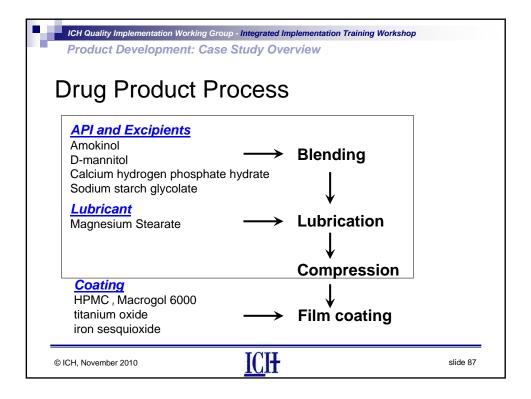


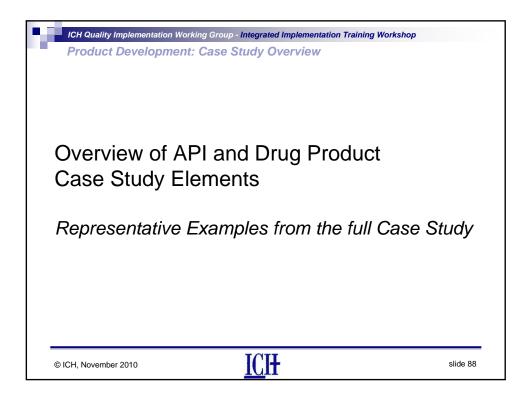


	Working Group - Integrated Implementation ent: Case Study Overview	n Training Workshop
	Product Profile (QTF	PP)
Tablet	Characteristics / Requirements	Translation into Quality Target Product Profile (QTPP)
Dose	30 mg	Identity, Assay and Uniformity
Subjective Properties	No off-taste, uniform color, and suitable for global market	Appearance, elegance, size, unit integrity and other characteristics
Patient Safety – chemical purity	Impurities and/or degradates below ICH or to be qualified	Acceptable hydrolysis degradate levels at release, appropriate manufacturing environment controls
Patient efficacy – Particle Size Distribution (PSD)	PSD that does not impact bioperformance or pharm processing	Acceptable API PSD Dissolution
Chemical and Drug Product Stability: 2 year shelf life (worldwide = 30°C)	Degradates below ICH or to be qualified and no changes in bioperformance over expiry period	Hydrolysis degradation & dissolution changes controlled by packaging
	le – during development and commercial m are identified, new technical information is	
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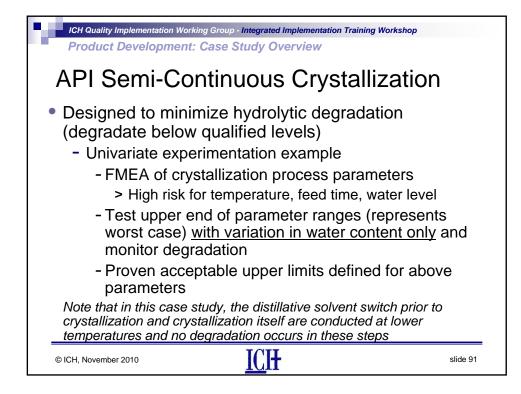
ICH Quality Implementation Working Group - Integrated Implementation Training Workshop Product Development: Case Study Overview									
Tablet Formulation									
Function	Specification	Excipient	Sakura Tablet 30 mg						
Active ingredient	Separate specification	Amokinol	30 mg / tablet						
	)		(100 mg)						
Excipient		Calcium hydrogen phosphate hydrate	Appropriate amount						
Excipient		D-mannitol	10 mg						
Disintegrant	Pharmacopoeial	Sodium starch glycolate	5 mg						
Lubricant	or other	Magnesium stearate	2 mg						
Coating agent	compendial	HPMC	2.4 mg						
Polishing agent	specification	Macrogol 6000	0.3 mg						
Coloring agent		Titanium oxide	0.3 mg						
Coloring agent	)	Iron sesquioxide	Trace amount						
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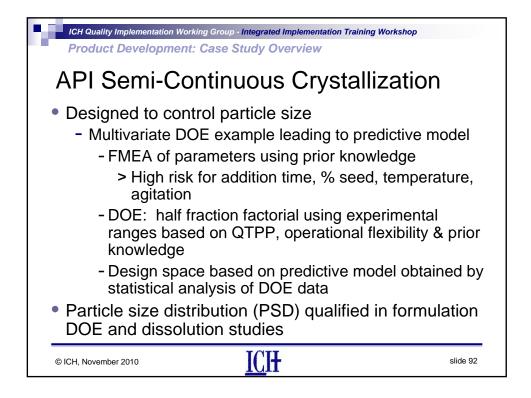




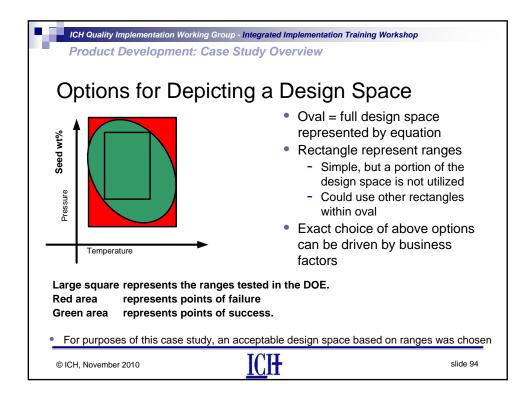
ICH Quality Implementation Working Group - Integrated Implementation Training Workshop           Product Development: Case Study Overview         Example from Case Study           Overall Risk Assessment for Process         Process Steps												
no impact to CQA     known or potential impact to CQA	Drug Substance Drug Product											
current controls mitigate risk     ektown or potential impact to COA     additional study required     includes bioperformace of API, and safety(API purity)     CQA	Coupling Reaction Aqueous Extractions Distillative Solvent Swrtch Semi- Continuous Continuous Continuous Continuous Filtration Rotary Drying						Manufacture Moisture Control	Blending	Lubrication	Compression	Coating	Packaging
in vivo performance*												
Dissolution												
Assay												
Degradation												
Content Uniformity												
Appearance												
Friability												
Stability-chemical												
Stability-physical												
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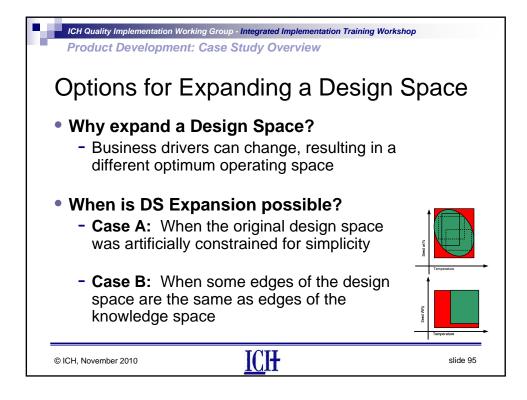
ICH Quality Implementation Working Group - Integrated Implementation Training Workshop           Product Development: Case Study Overview           Overall Risk Assessment for Process           Process Steps													
	potential impact to CQA	Drug Substance Drug Product											
<ul> <li>known or j</li> <li>additional</li> </ul>	Introls mitigate risk potential impact to CQA study required vioperformace of API, and purity) CQA	Coupling Reaction	Coupling Reaction Aqueous Extractions Distillative Solvent Switch Semi- Continuous Continuous Continuous Filtration Filtration Rotary Drying						Blending	Lubrication	Compression	Coating	Packaging
	in vivo performance*												
	Dissolution												
	Assay												
	Degradation												
	Content Uniformity												
	Appearance												
	Friability												
	Stability-chemical												
	Stability-physical												
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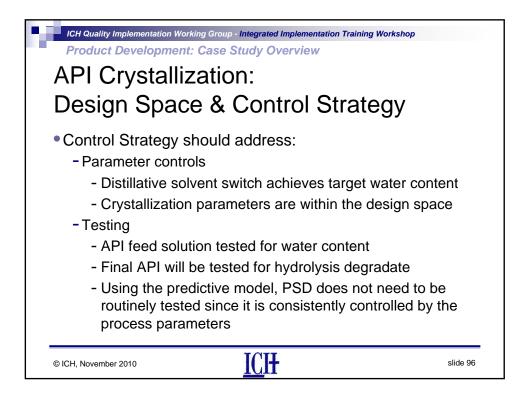




Product D Risk A Particle	Development: Case SSESSMEN Size Distribu	st nt: itic	br	לא אר ו	01 (P	
What is our Ability to Dete Unit Operation	Parameter			7	aningf	ful control point? 1) certain 5) moderate 9) unlikely Comments
Crystallization	Feed Temperature	1	5		5	Prior knowledge (slowness of crystallization kinetics) ensures that the hot crystallizer feed will be well discussed and themelie availisated before crystallizing. Hence no irr <b>To be investigated</b> crystal size.
Crystallization	Water content of Feed	1	5	5	25	Prior knowledge (solubility data) in DOE do not affect crystalliation whetics.
Crystallization	Addition Time (Feed Rate)	9	5	9	405	Fast addition could result in unconfolled crystallization. Detection of short addition time could occur too late to prevent this uncontrolled crystallization, and thus impact final PSD.
Crystallization	Seed wt percentage	9	5	5	225	Prior knowledge (Onemical Engineering theory) highlights seed wt percentage variations as a potential source of final PSD variation
Crystallization	Antisolvent percentage	1	1	1	1	Yield loss to crystallization already low (< 5%), so reasonable variations in antiscivent percentage (+/- 10%) will not affect the percent of batch crystallized, and will not affect PSD
Crystallization	Temperature	9	5	9	405	Change in crystallization temperature is easily detected, but rated high since no possible corrective action (such as, if seed has been dissolved)
Crystallization	Agitation (tip speed)	9	5	5	225	Prior knowledge indicates that final PSD highly sensitive to Agitation, thus requiring further study.
Crystallization	Seed particle size distribution	9	1	1	9	Seed PSD controlled by release assay performed after air attrition milling
Cr <u>vstallization</u> © ICH, November 2	Preut Concentration		I	C	H	Same logic as for antisolvent percentage







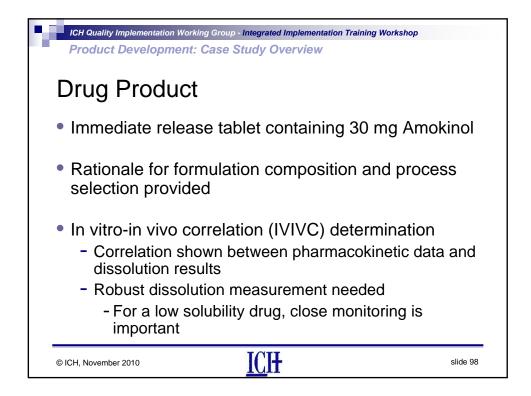
Particle Size	Crystallization	Temperature	20 to 30°C	Control between 23 and 27°C
Particle Size	Crystallization	Feed Time	5 to 15 hours	Control via flow rate settings
Particle Size	Crystallization	Agitation	1.1 to 2.5 m/s	Quality system should ensure changes in agitator size result in change to speed setting
Particle Size	Crystallization	Seed Wt%	1 to 2 wt%	Controlled through weigh scales and overcheck
Hydrolysis Degradate	Distillation / Crystallization	Water Content	< 1 vol%	Control via in-process assay

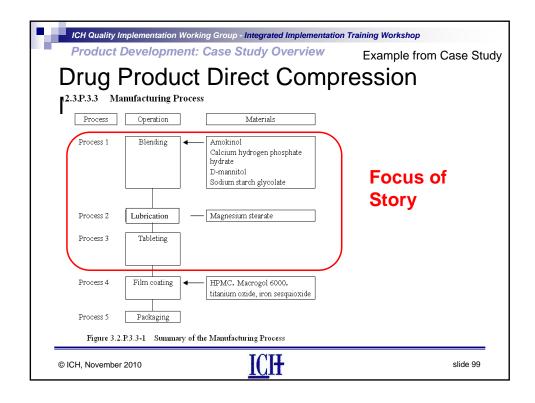
ICH Quality Implementation Working Group - Integrated Implementation Training Workshop

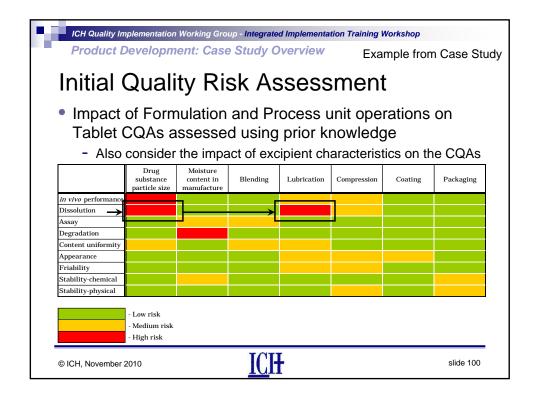
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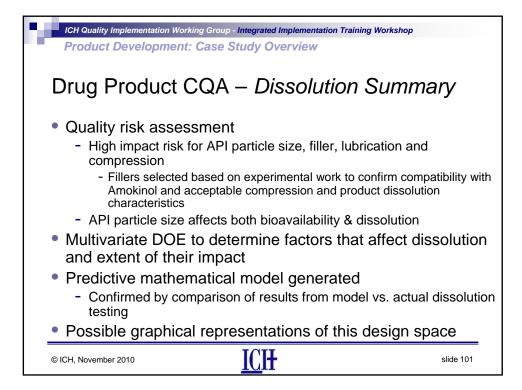
Example from Case Study

Product Development: Case Study Overview

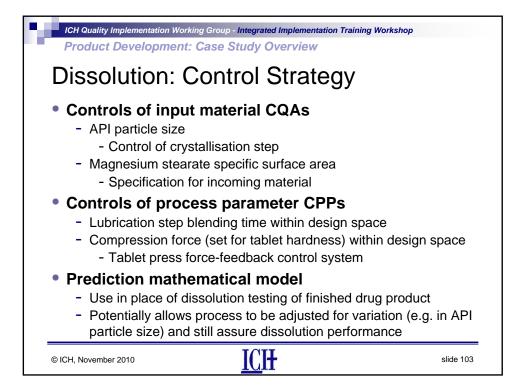


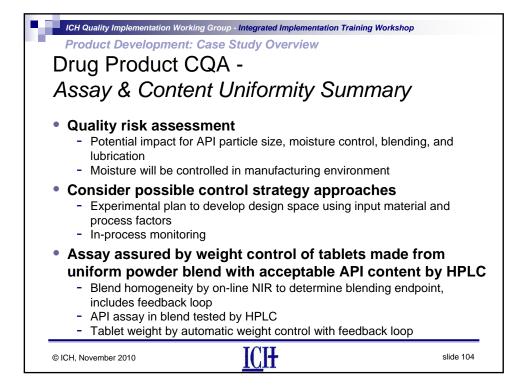


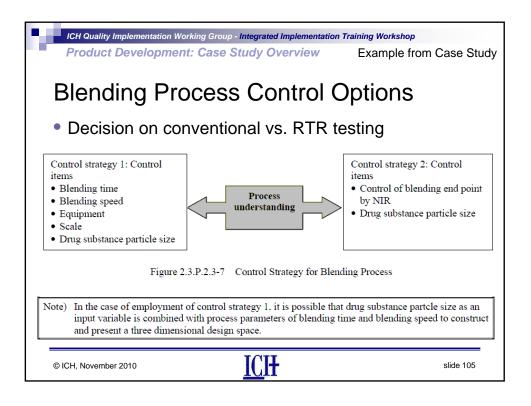


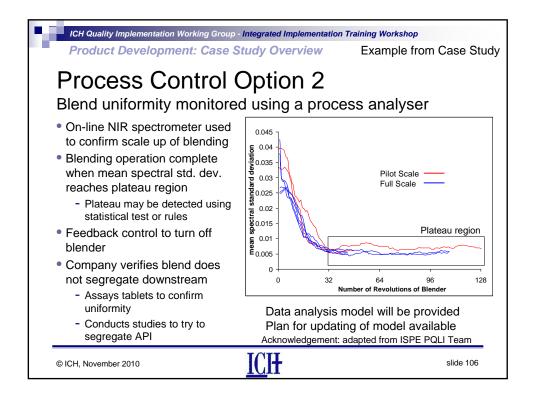


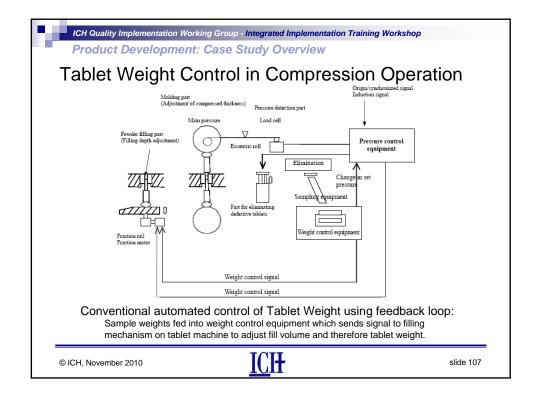
ICH Quality Implementation Wo	orking Group - Integrate	d Implementation Training	g Workshop
Product Developmen	t: Case Study C	<b>)verview</b> Ex	ample from Case Stud
Predictive Mo			space
<b>Prediction algorith</b> Diss = 108.9 - 11.96 3.783×10 <sup>-2</sup> × Hard -	3 × API – 7.556		0.1849 × LubT –
Factors include: API surface area, lubricati	on time, tablet	· •	<i>,</i> , ,
	Batch 1	Batch 2	Batch 3
Model prediction	89.8	87.3	88.5
Dissolution testing result	92.8 (88.4–94.2)	90.3 (89.0-102.5)	91.5 (90.5-93.5)
Continue model verification	with dissolution	testing of production	on material, as needed
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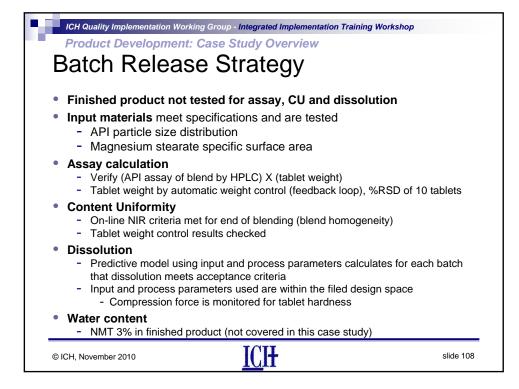


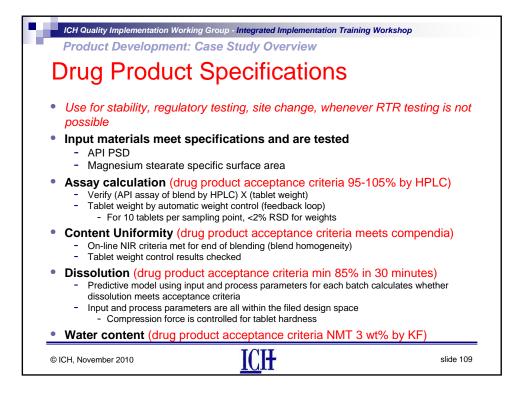


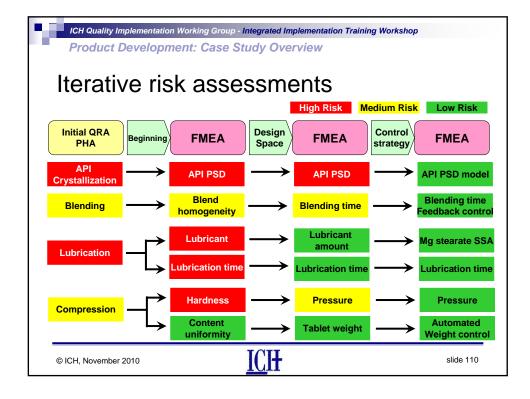


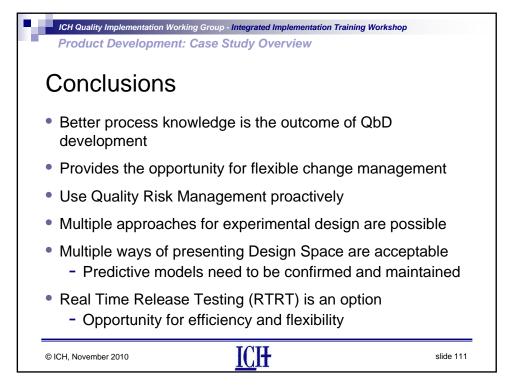


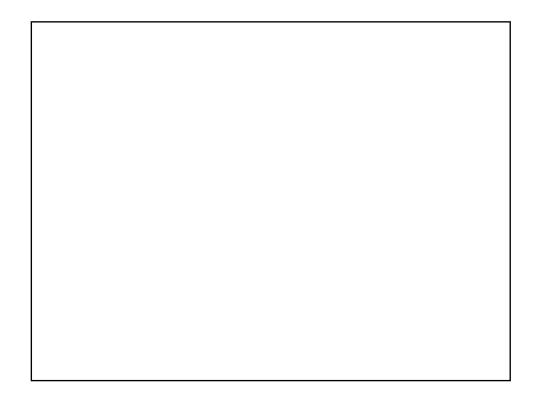


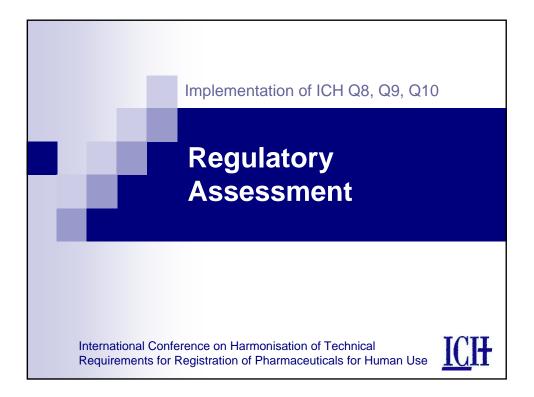






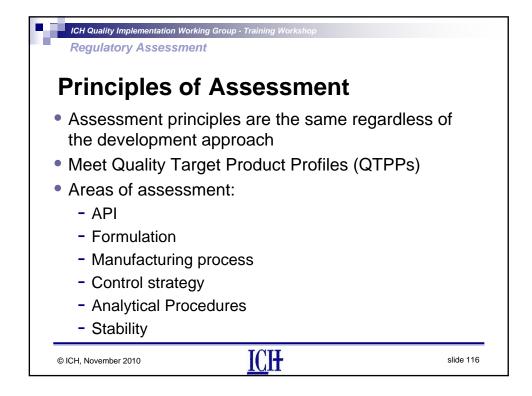


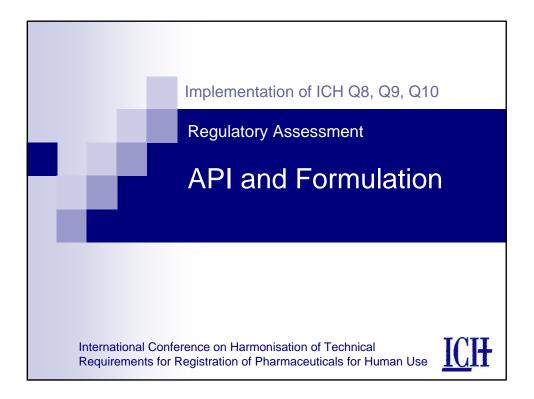


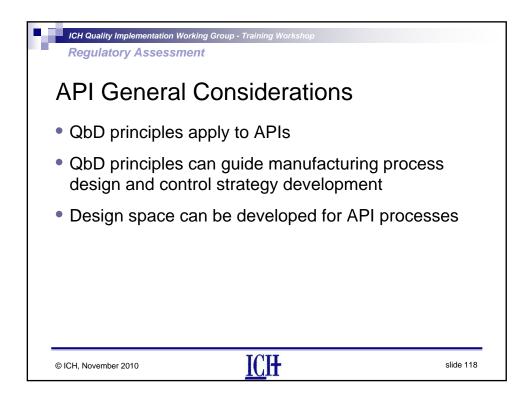


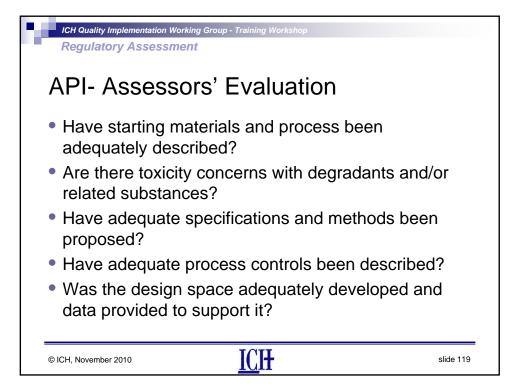
ICH Quality Implementation Working Group - Training Workshop Regulatory Assessment
Presentation Overview
<ul> <li>Goal of Regulatory Quality Assessment</li> </ul>
<ul> <li>Review of the case study         <ul> <li>Considerations during regulatory evaluation</li> <li>Areas of consideration by assessors will be presented in the form of questions for the assessor</li> <li>The questions presented here are not necessarily the ones which are finally communicated in regulatory deficiency letters</li> </ul> </li> <li>API and Formulation</li> <li>Manufacturing Process Development         <ul> <li>Quality Risk Management</li> <li>Design Space</li> </ul> </li> <li>Proposed Control Strategy         <ul> <li>Assessors - Inspector Interaction</li> </ul> </li> </ul>
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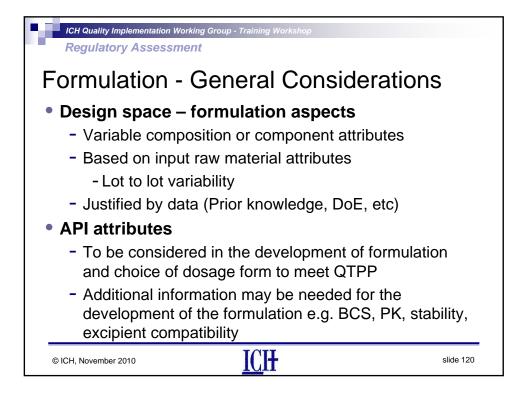


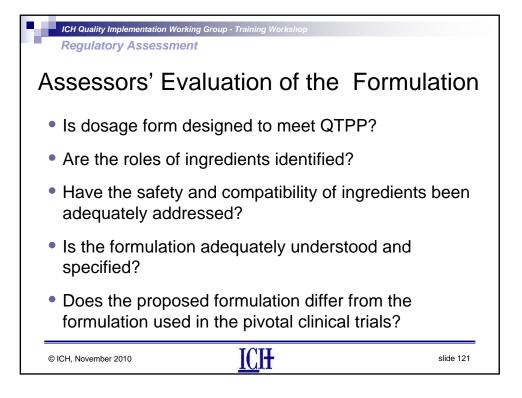


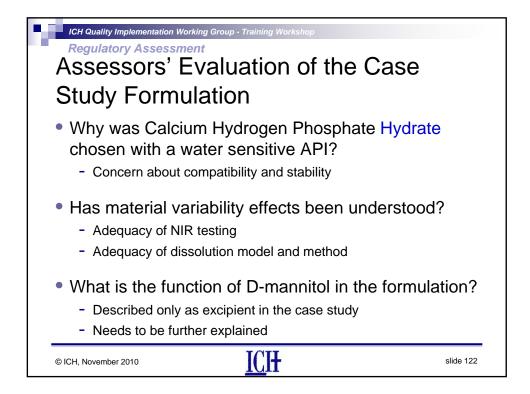






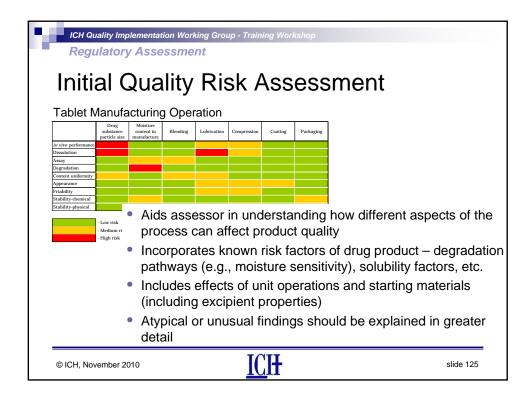


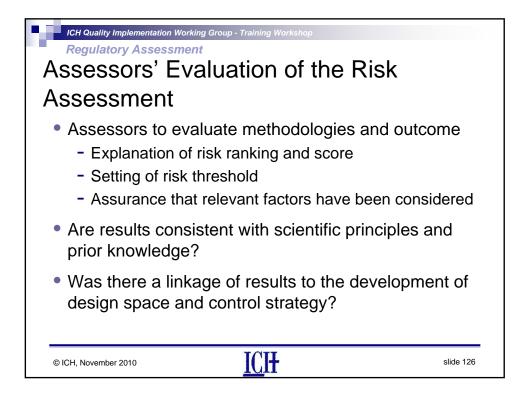


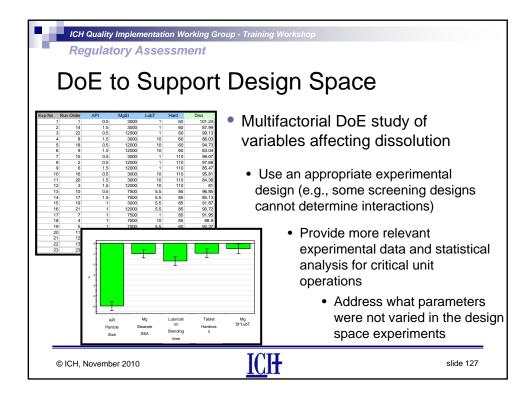


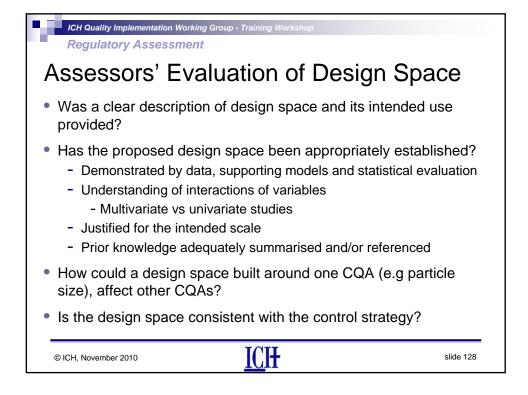


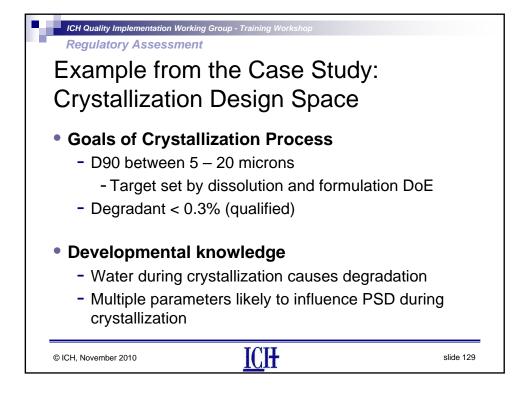


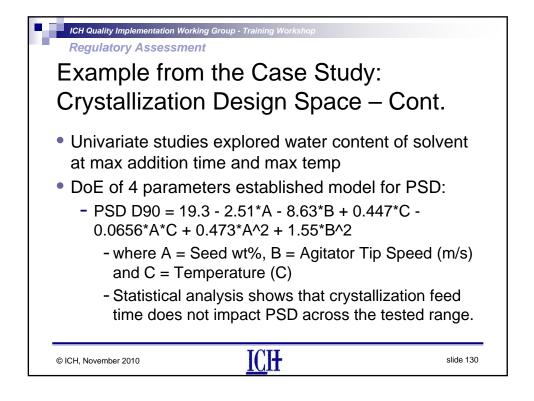


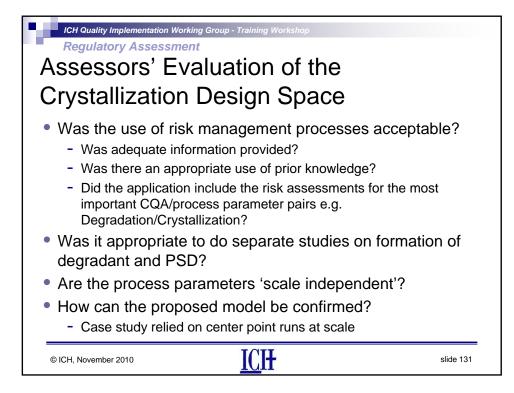


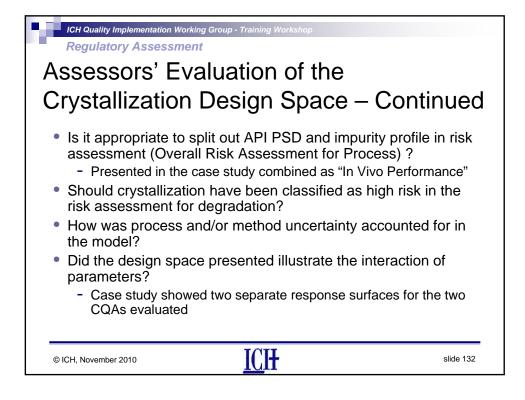




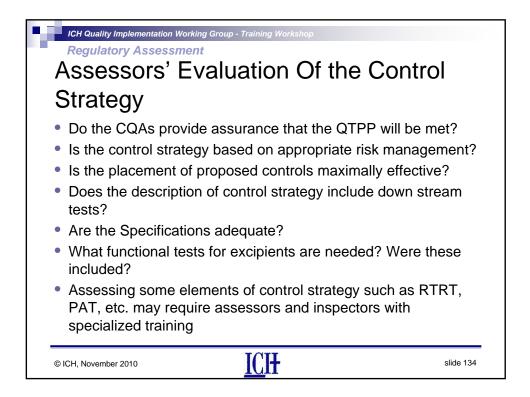


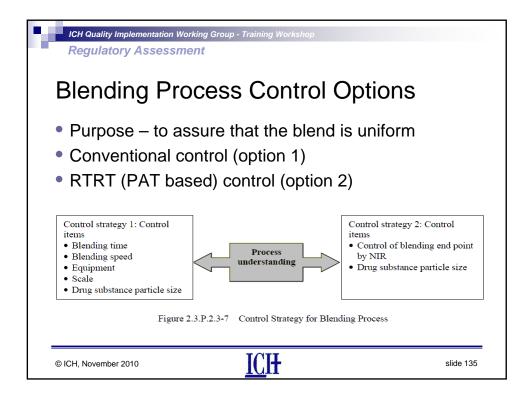


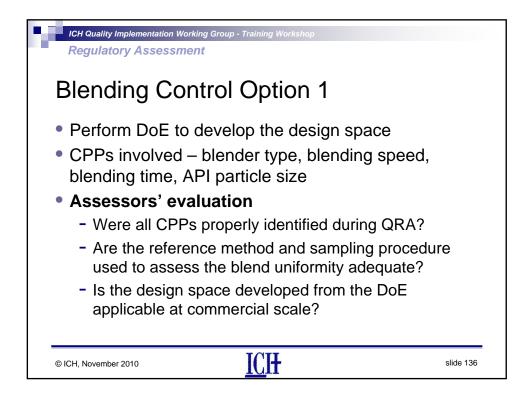


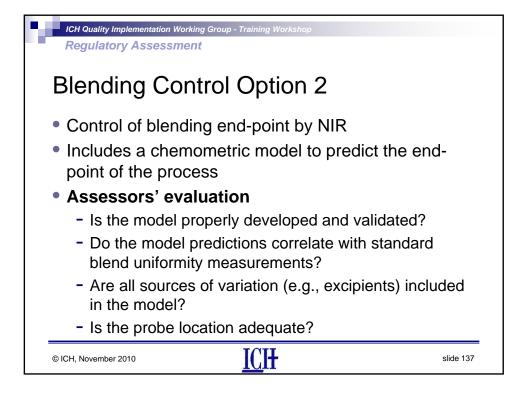


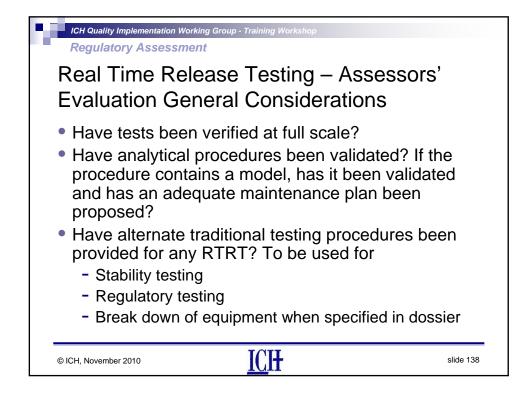


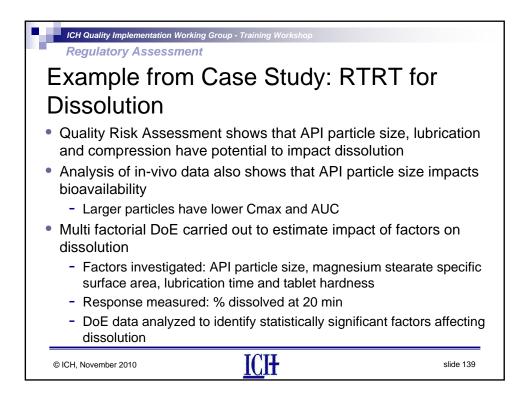


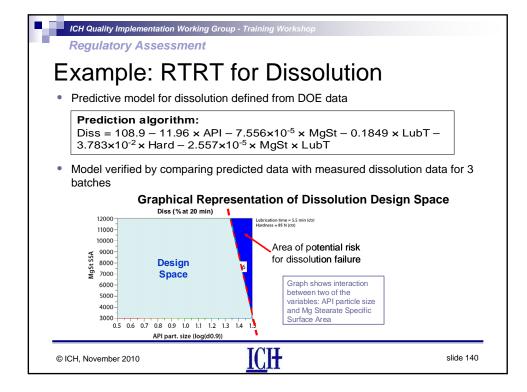


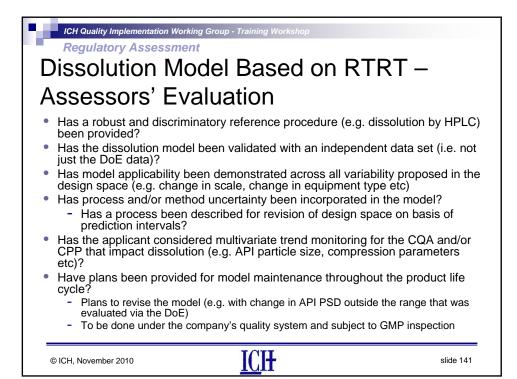


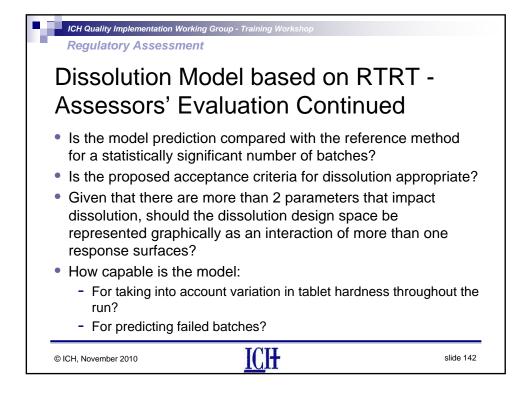


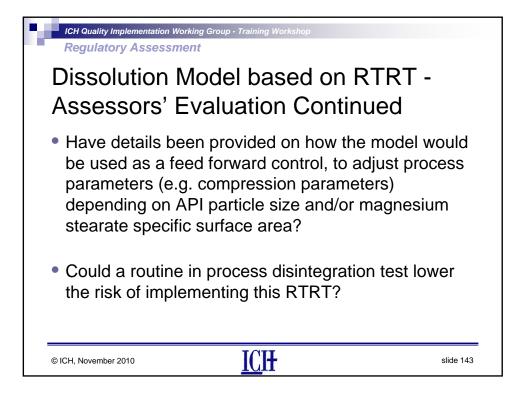


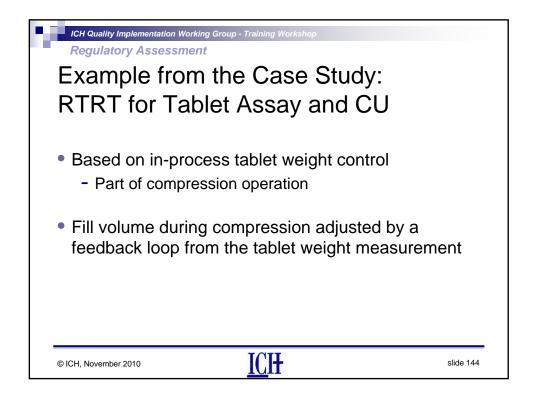


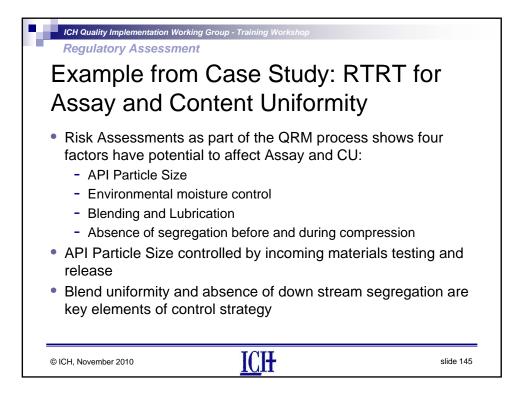


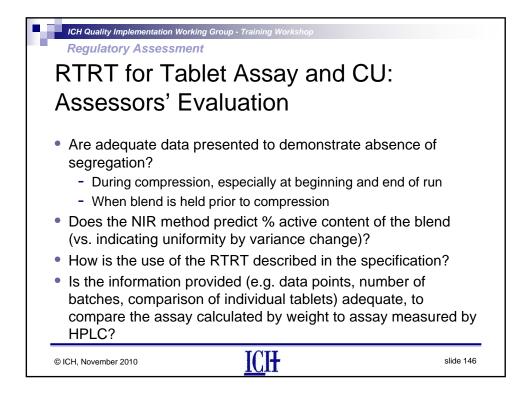


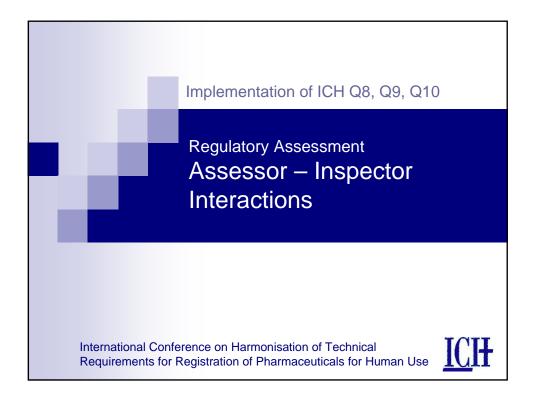


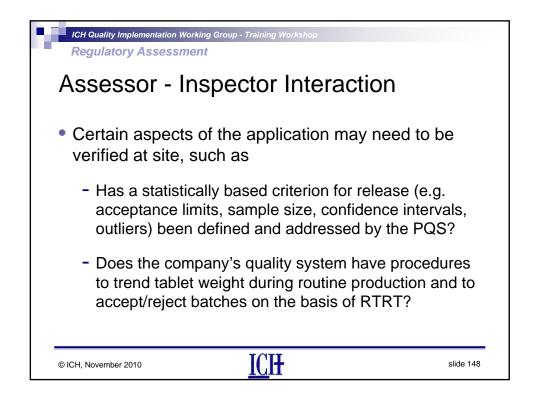


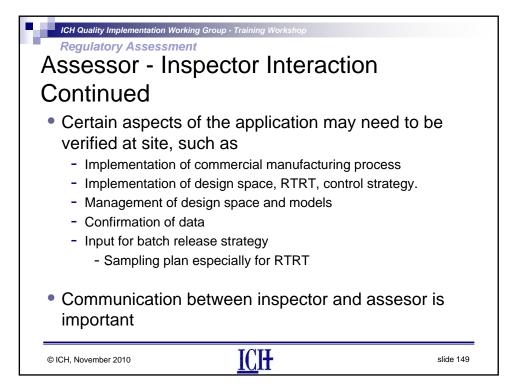


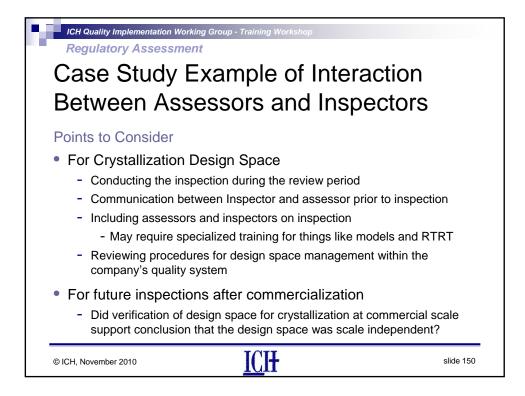


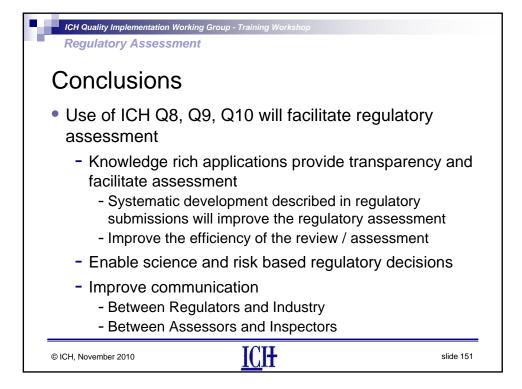






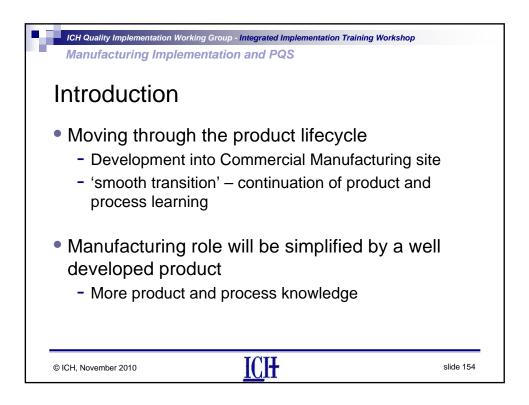


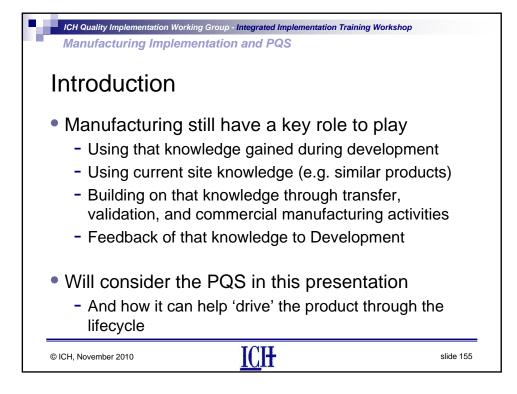


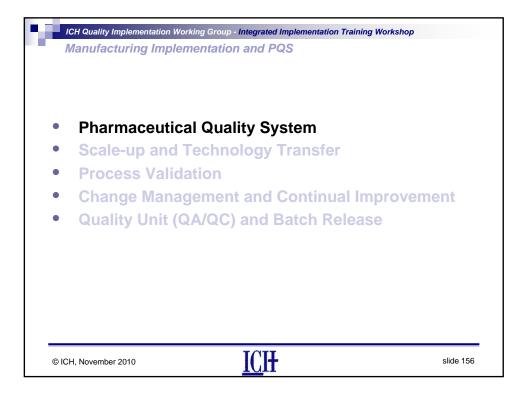


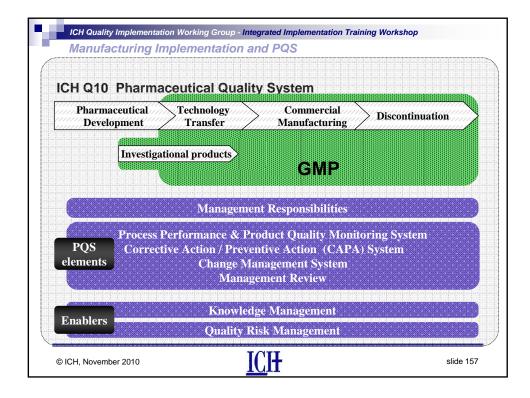


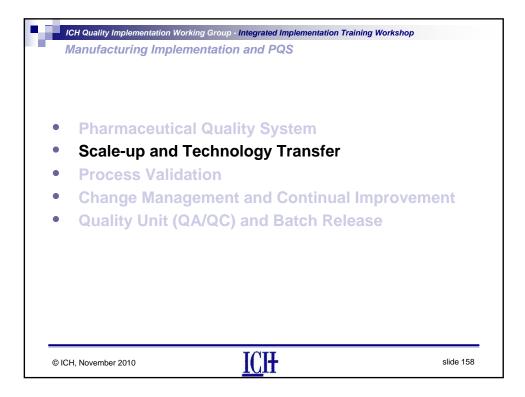


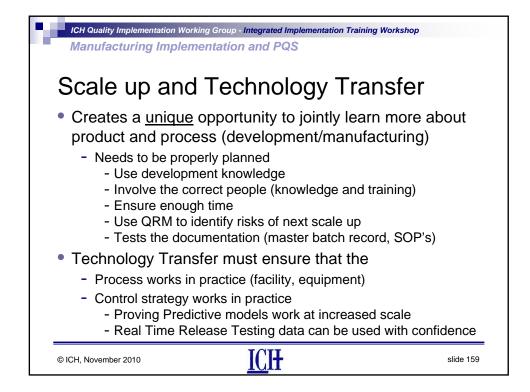


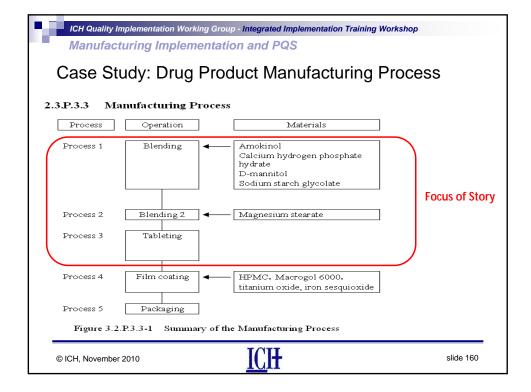


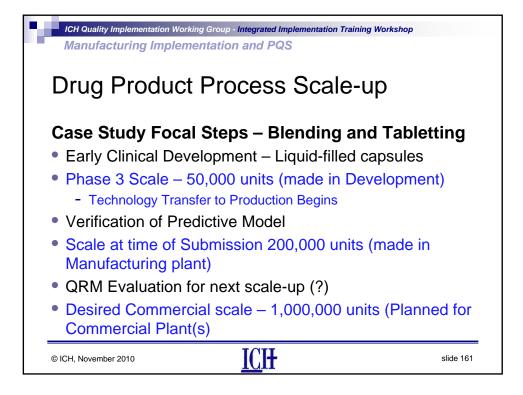


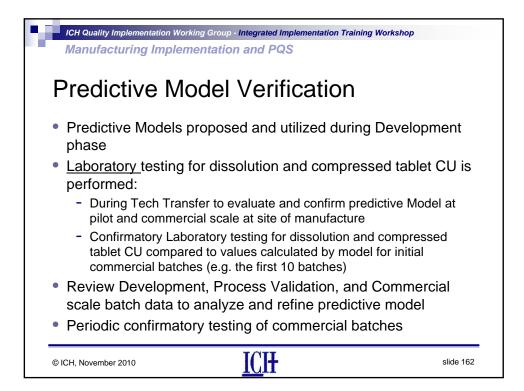


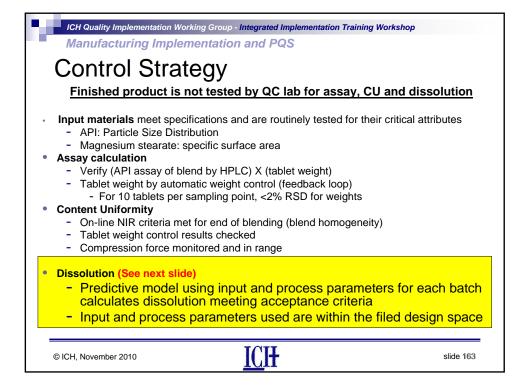






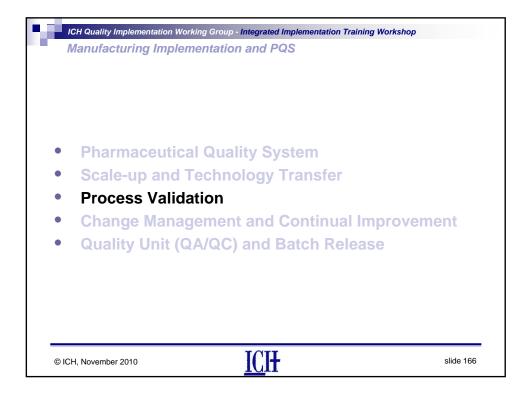


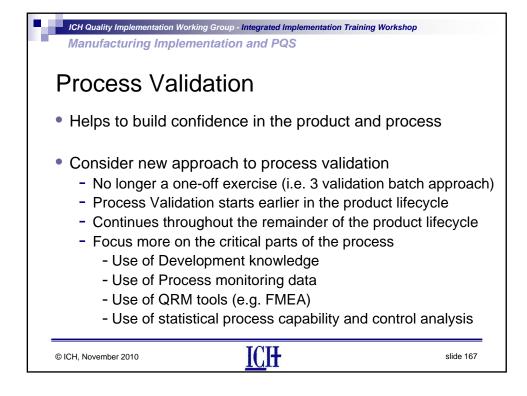


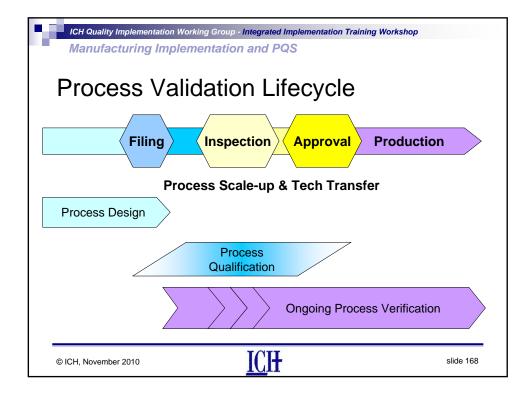


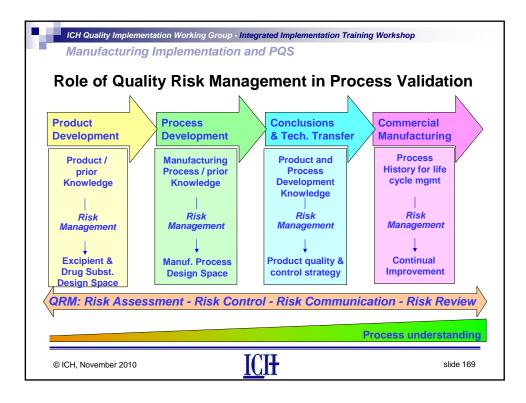
		rking Group - Integrated I mentation and PG	mplementation Training Worksho	qq					
	ution: Contro	_							
Material Inputs	API PSD Crystallizatio		Magnesium Stearate Sp. Surface Area (MgSt) Supplier Control / Specification						
Process Steps		Blending	Lube Time (LT)	Predictive Model					
		Tableting	Hardness (HARD)						
Finished Product	<u>Algor</u>	ithm Calculation	[DISS = F(MgSt, LT,	API, HARD)]					
	↓ Calculated Dissolution Result (No testing required)								
		s process to be adjusted for sure dissolution performanc							
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Predictive Model for Dissolution           Prediction algorithm:           Diss = 108.9 - 11.96 × API - 7.556×10 <sup>-5</sup> × MgSt - 0.1849 × LubT - 3.783×10 <sup>-2</sup> × Hard - 2.557×10 <sup>-5</sup> × MgSt × LubT												
	Factors include: API PSD, magnesium stearate specific surface area, lubrication time, tablet hardness Confirmation of model											
		Batch 1	Batch 2	Batch 3								
	Model prediction	89.8	87.3	88.5								
	Dissolution testing result	92.8 (88.4–94.2)	90.3 (89.0-102.5)	91.5 (90.5-93.5)								
				No failures. Verify model in production scale to determine if it provides suitable and sufficient surrogate to replace direct measurement of the critical product attribute (dissolution). The model will be maintained within the PQS								
su	ifficient surrogate to repla	ace direct measu	urement of the critica									

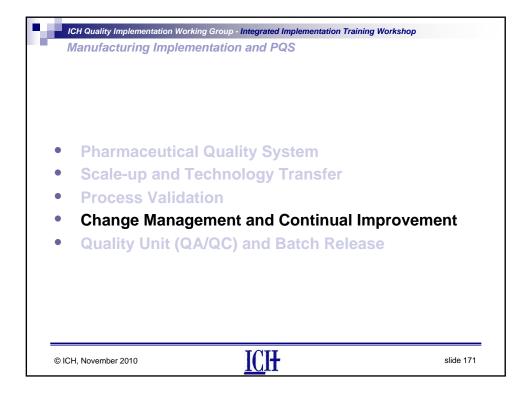


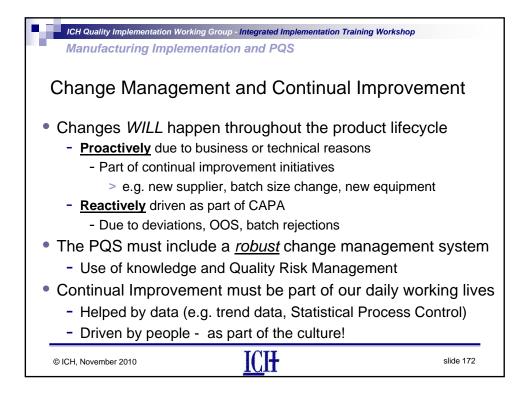


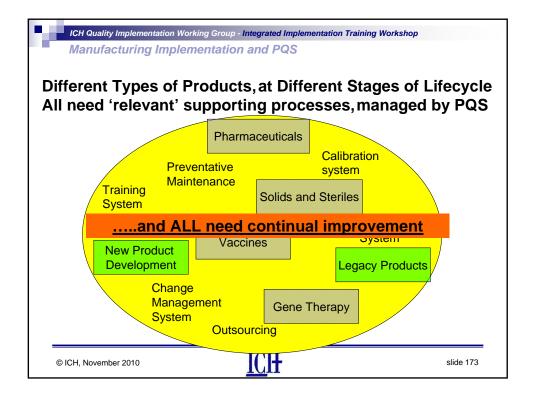


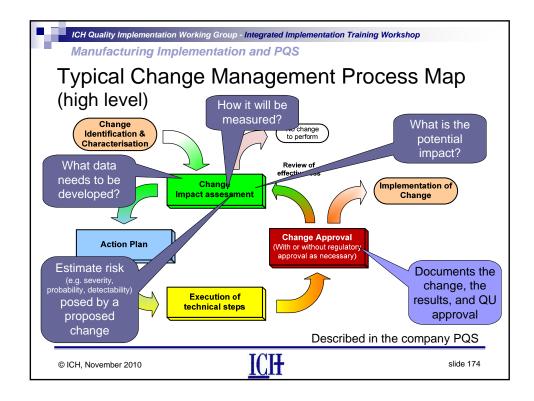


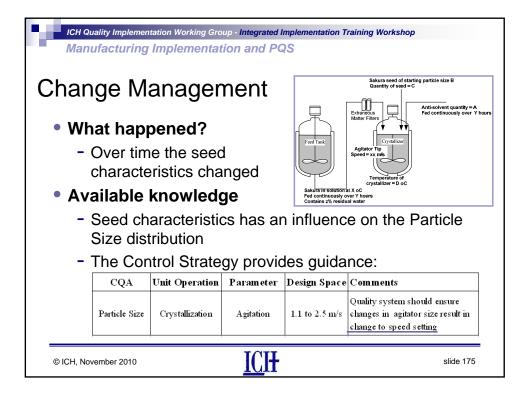


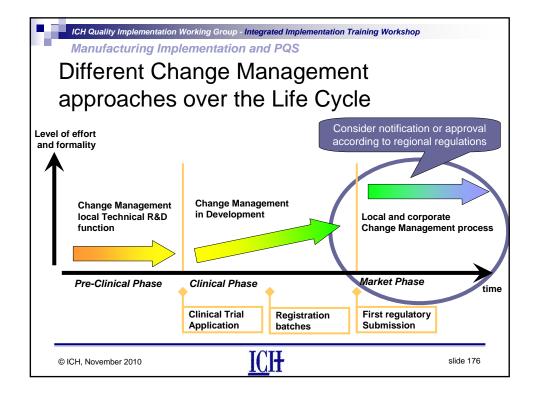


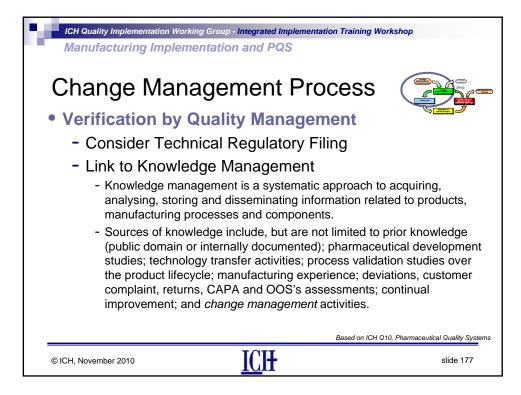


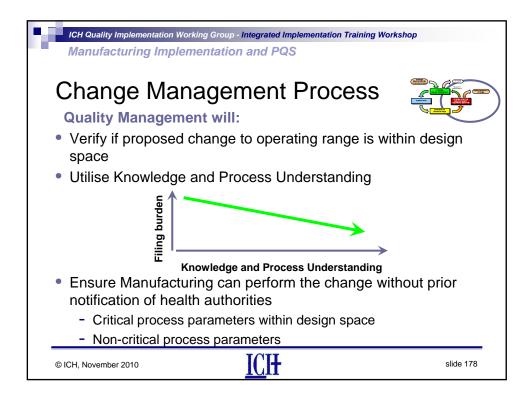


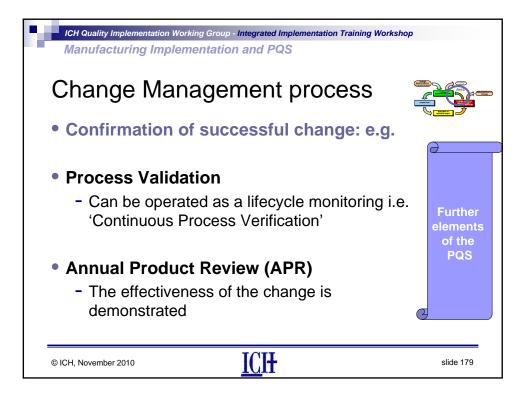


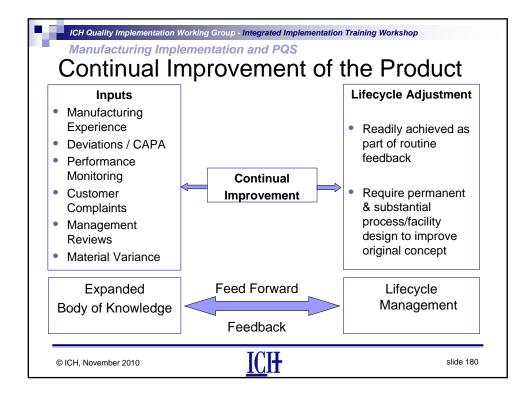


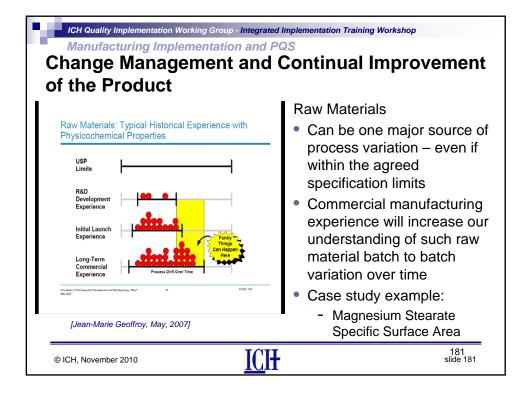


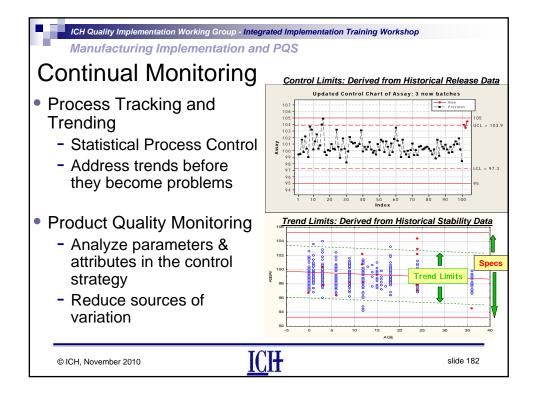




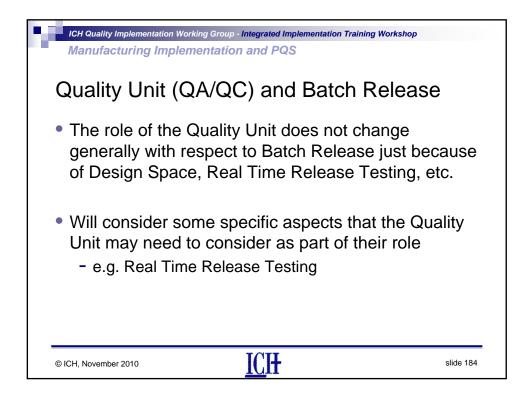






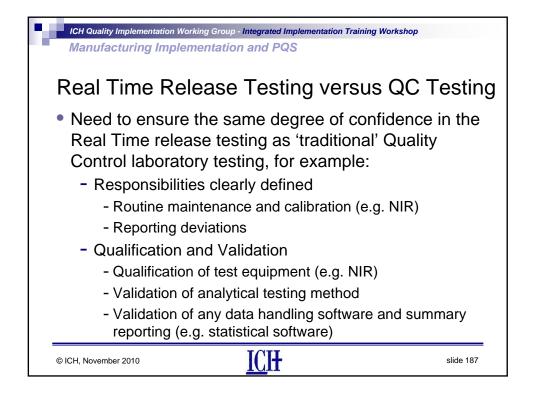


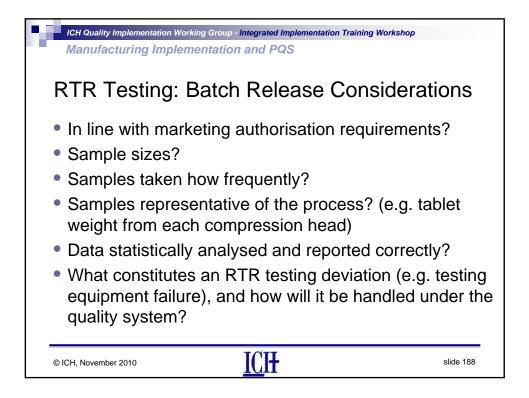


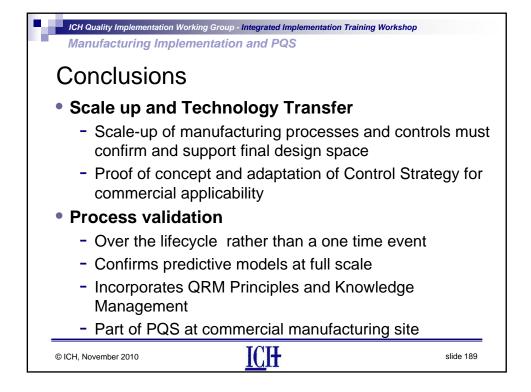


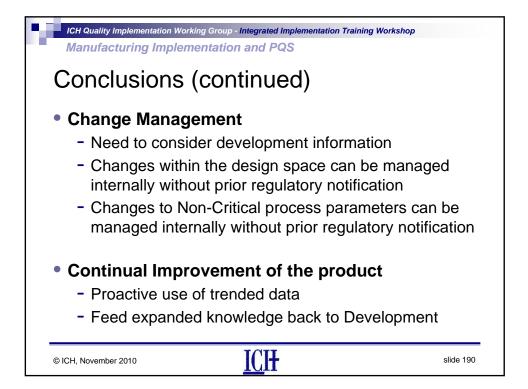


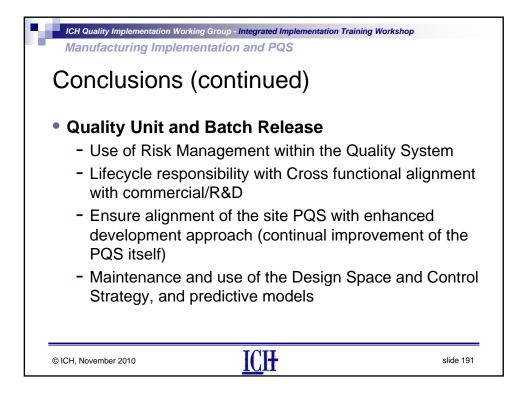


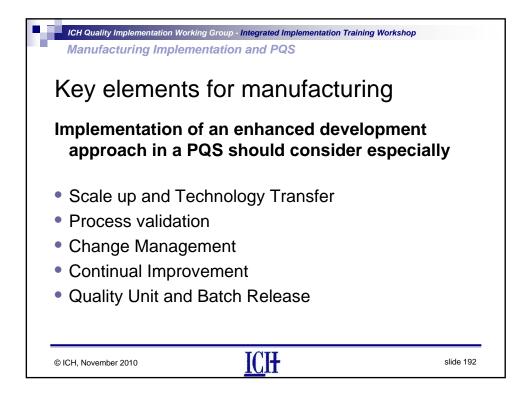


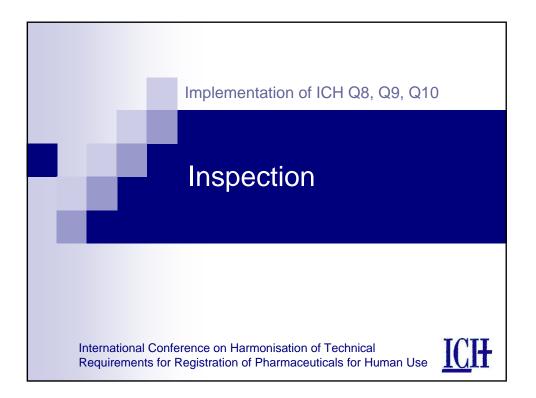


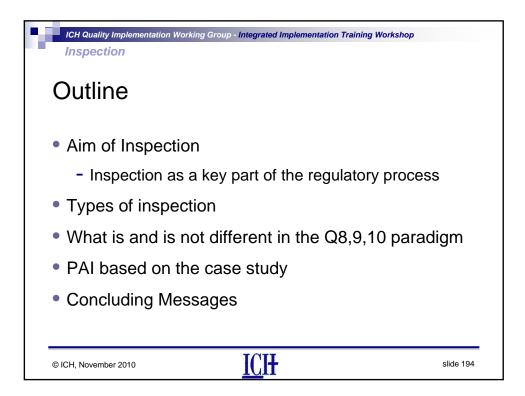




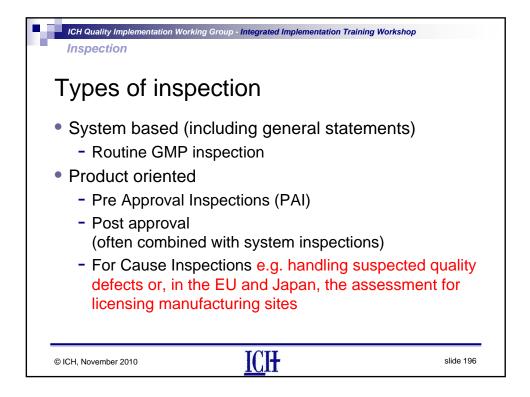


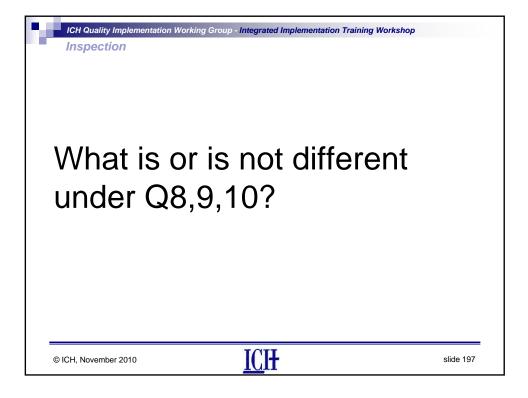


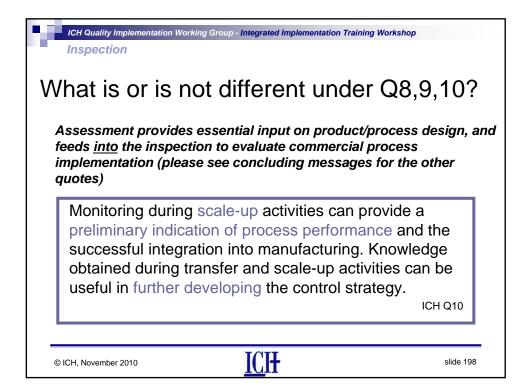


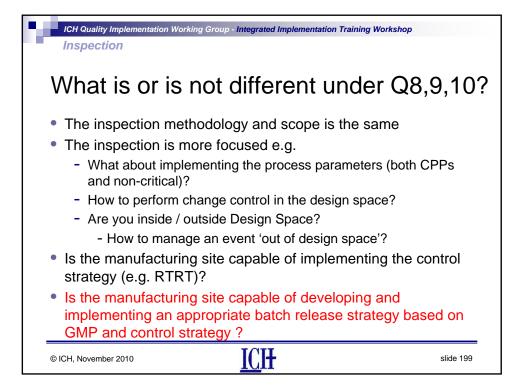


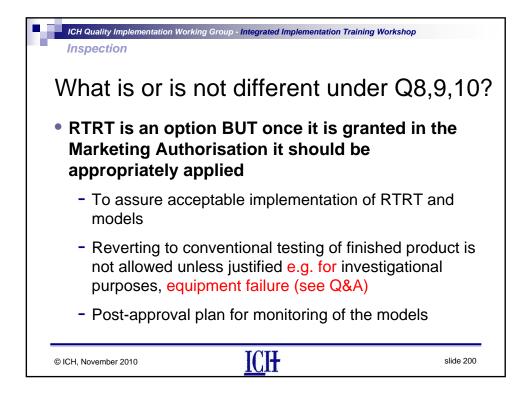
ICH Quality Implementation Working Group - Integrated Implementation Training Workshop
Aim of the inspection
Inspections of a firm's manufacturing operation are essential to evaluate commercial manufacturing capability, adequacy of production and control procedures, suitability of equipment and facilities, and effectiveness of the quality system in assuring the overall state of control. Notably, pre-approval inspections include the added evaluation of authenticity of submitted data and link to dossier.
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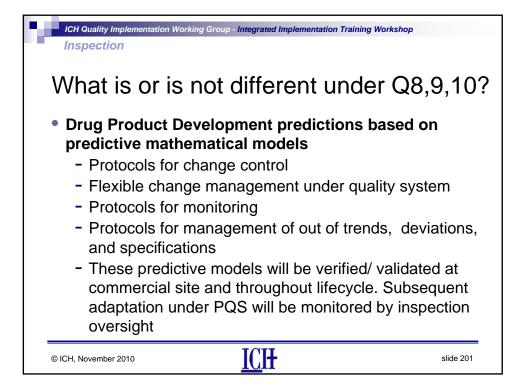


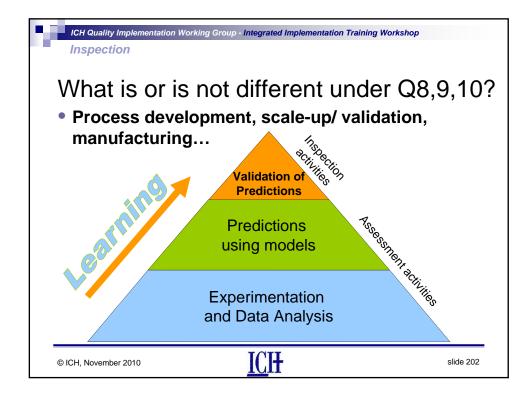


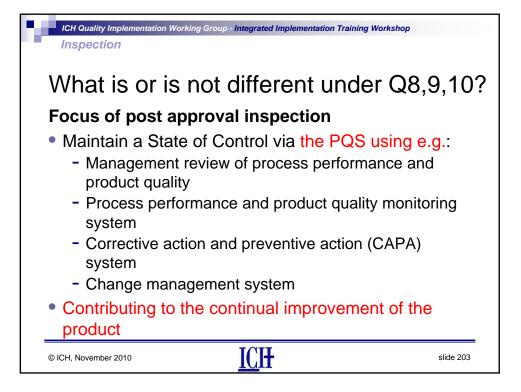


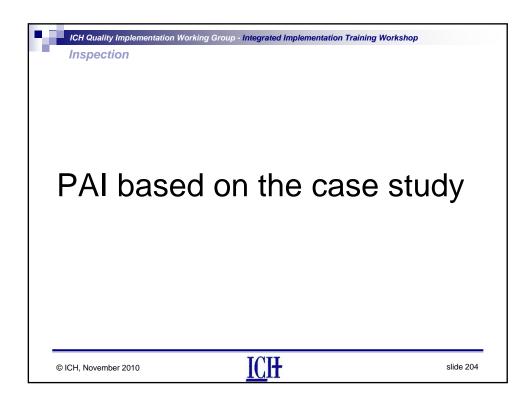


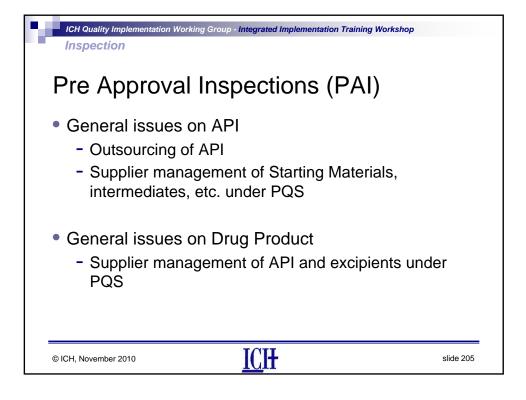


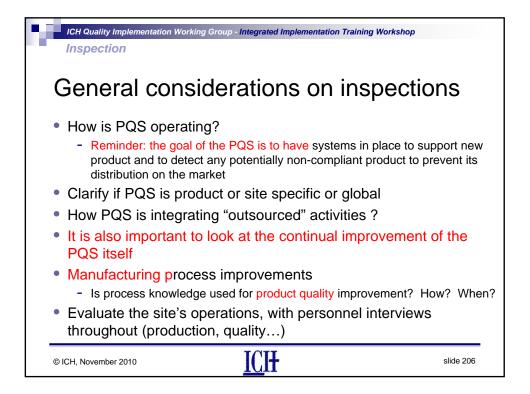


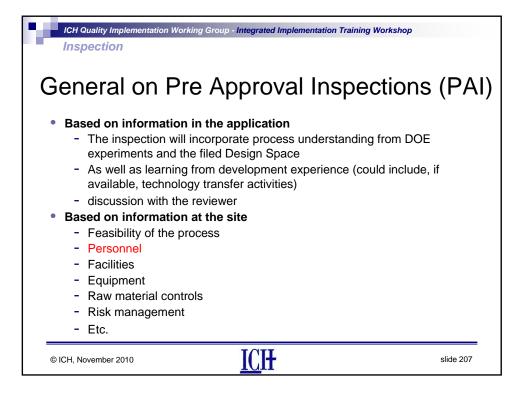


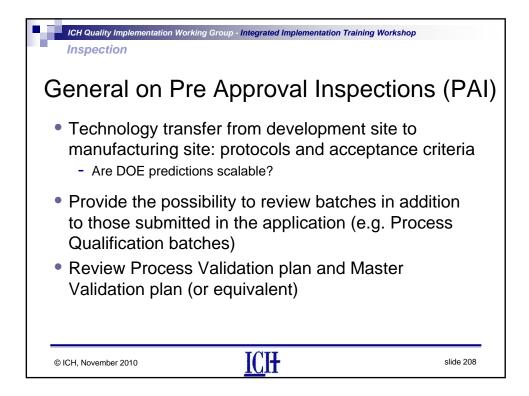


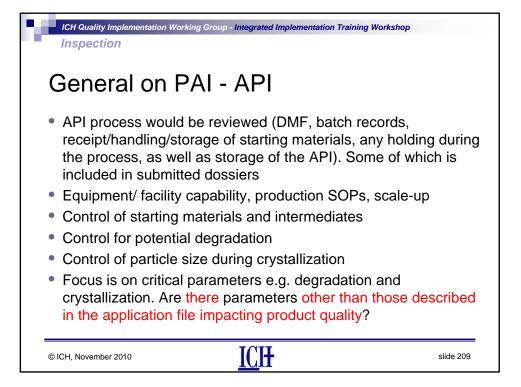


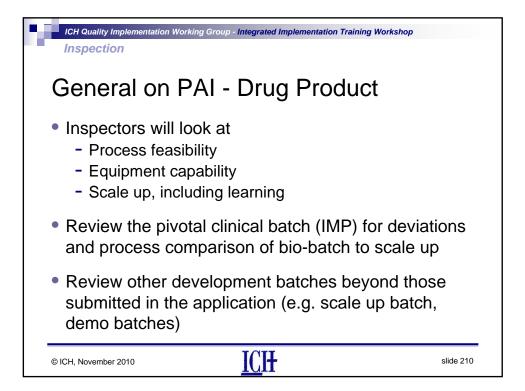


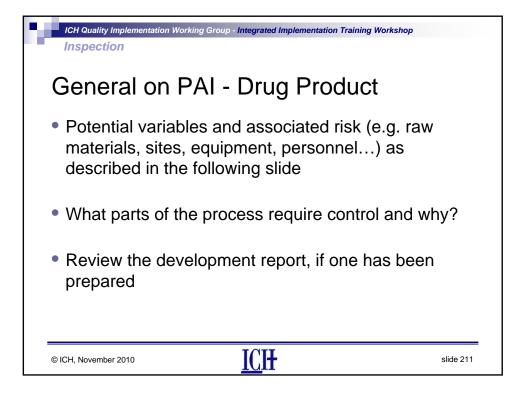


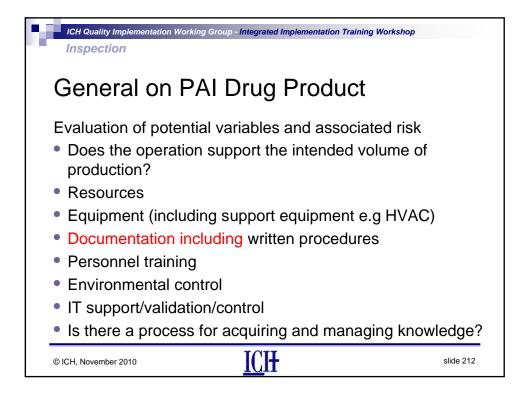


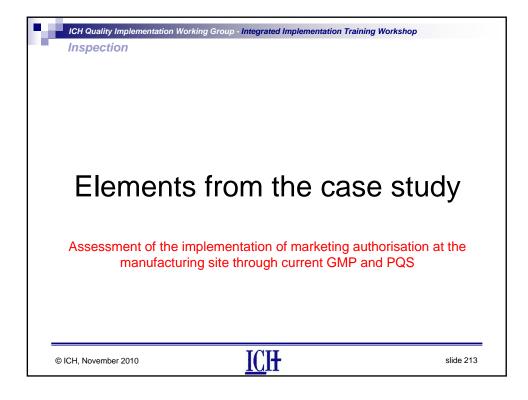












ICH Quality Implementation Working Group - Integrated Implementation Training Workshop Inspection Overall Risk Assessment for Process											
	Process Steps										
	Drug Substance					Drug Product					
Coupling Reaction	Aqueous Extractions	Distillative Solvent Switch	Semi-Continuous Crystallization	Centrif ugal Filtration	Rotary Drying	Manufacture Moisture Control	Blending	Lubrication	Compression	Coating	Packaging
Stability-physical											
	Ris	Risk A	Risk Ass	Risk Asses	Risk Assessm Pro	Risk Assessmen Proces	Risk Assessment fo Process Step	Risk Assessment for P Process Steps Drug Substance D	Risk Assessment for Proc Process Steps Drug Substance Drug P	Risk Assessment for Proces Process Steps Drug Substance Drug Produc	Risk Assessment for Process Process Steps Drug Substance Drug Product

