

Lecture 5 – Sampled Time Control

- Sampled time vs. continuous time: implementation, aliasing
- Linear sampled systems modeling refresher, DSP
- Sampled-time frequency analysis
- Sampled-time implementation of the basic controllers
 - I, PI, PD, PID
 - 80% (or more) of control loops in industry are digital PID

Sampled Time Models

- Time is often sampled because of the digital computer use
 - digital (sampled time) control system

$$x(t + d) = f(x, u, t)$$

$$y = g(x, u, t)$$

- Numerical integration of continuous-time ODE

$$x(t + d) \approx x(t) + d \cdot f(x, u, t), \quad t = kd$$

- Time can be sampled because this is how a system works

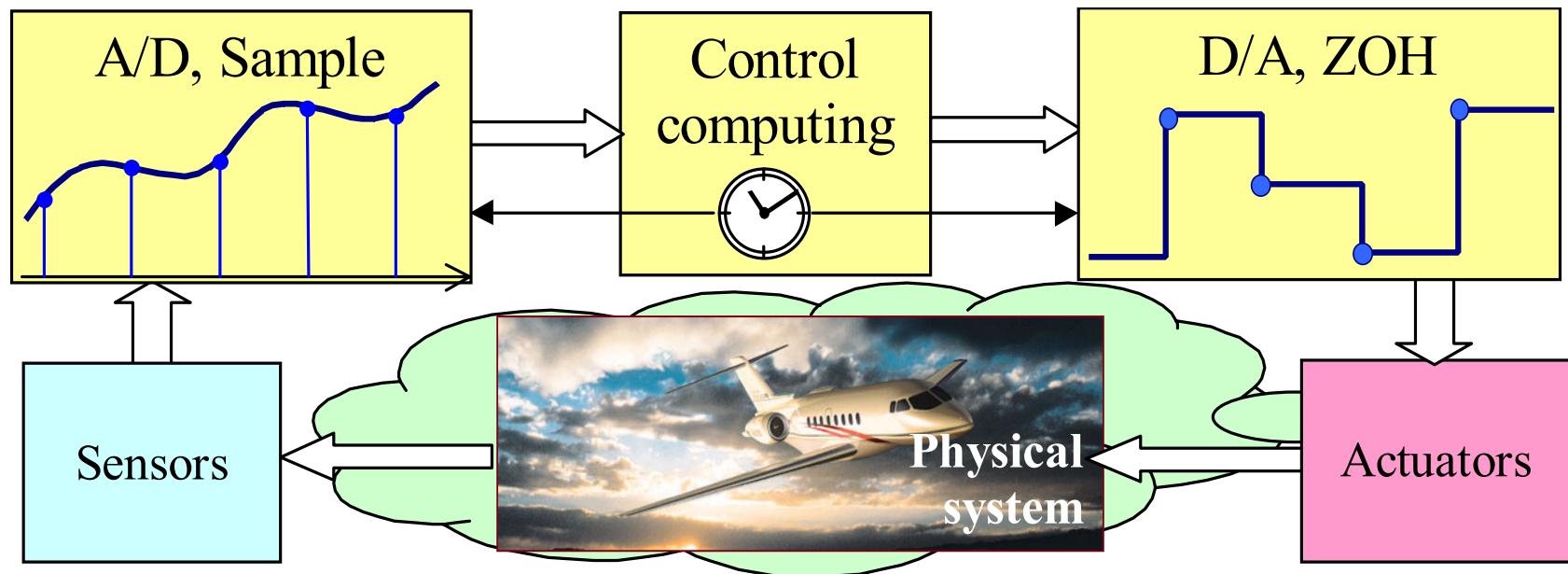
- Example: bank account balance

- $x(t)$ - balance in the end of day t
- $u(t)$ - total of deposits and withdrawals that day
- $y(t)$ - displayed in a daily statement

$$\boxed{\begin{aligned} x(t+1) &= x(t) + u(t) \\ y &= x \end{aligned}}$$

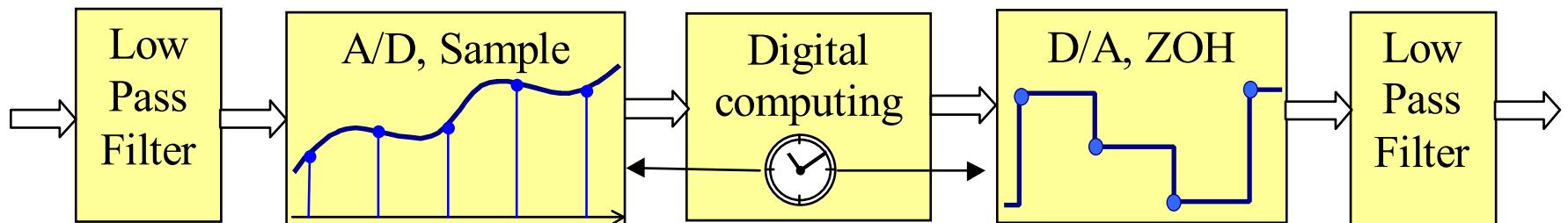
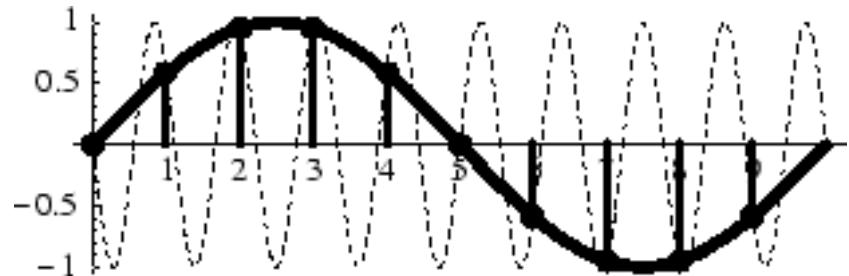
Sampling: continuous time view

- Sampled and continuous time together
- Continuous time physical system + digital controller
 - ZOH = Zero Order Hold



Signal sampling, aliasing

- Nyquist frequency:
 $\omega_N = \frac{1}{2}\omega_S; \omega_S = 2\pi/T$
- Frequency folding: $k\omega_S \pm \omega$ map to the same frequency ω
- Sampling Theorem: sampling is Ok if there are no frequency components above ω_N
- Practical approach to anti-aliasing: low pass filter (LPF)
- Sampled → continuous: impostoring



Linear state space model

- Generic state space model:

$$x(t+1) = f(x, u, t)$$

$$y = g(x, u, t)$$

- LTI state space model

- Physics-based linear system model
- Obtained by sampling a continuous time model
- Zero-order hold (ZOH)

$$\dot{x}(t) = A_c x(t) + B_c u(t)$$

$$y(t) = C_c x(t)$$

$$\boxed{\begin{aligned} x(t+1) &= Ax(t) + Bu(t) \\ y(t) &= Cx(t) \end{aligned}}$$

$$x(t+T) = \underbrace{e^{A_c T} x(t)}_A + \underbrace{\left(\int_0^T e^{A_c t} B_c dt \right) u(t)}_B$$

$$y(t) = C_c x(t)$$

- Matlab commands for model conversion: **help ltimodels**

Disk read-write head example

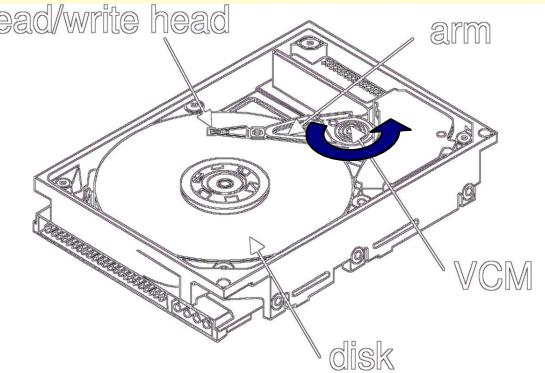
- Sampled time model for $T=0.0001$
(use Matlab `ss` and `c2d`)

$$x(k+1) = \underbrace{\begin{bmatrix} 0.998 & 0 \\ 10^{-4} & 0 \end{bmatrix}}_A \cdot x(k) + \underbrace{\begin{bmatrix} 10^{-3} \\ 5 \cdot 10^{-8} \end{bmatrix}}_B \cdot u(k)$$

$$y(k) = \underbrace{\begin{bmatrix} 0 & 1 \end{bmatrix}}_C \cdot x(k)$$

$x(k+1)$	$= Ax(k) + Bu(t)$
$y(k)$	$= Cx(k)$

Read-write head control



$$\ddot{y} + b\dot{y} = gu \quad b = 20, g = 10$$

$$y = \frac{10}{s(s+20)} u$$

$$\frac{dx}{dt} = \underbrace{\begin{bmatrix} -20 & 0 \\ 1 & 0 \end{bmatrix}}_A \cdot x + \underbrace{\begin{bmatrix} 10 \\ 0 \end{bmatrix}}_B \cdot u$$

$$y = \underbrace{\begin{bmatrix} 0 & 1 \end{bmatrix}}_C \cdot x$$

Sampled-time system stability

$$x(k+1) = Ax(k), \quad x(0) = x_0$$

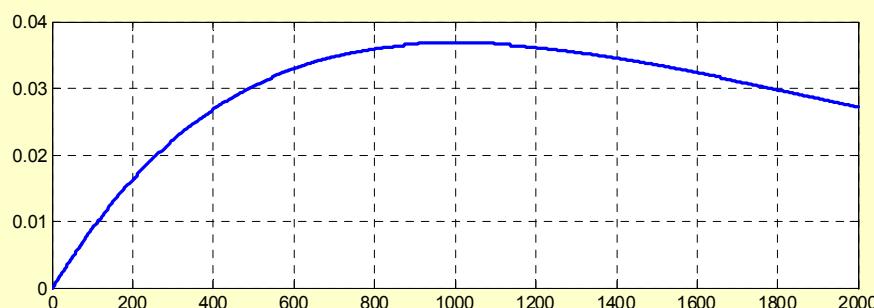
- Initial condition response

$$x(k) = A^k x_0$$

- Exponential stability condition

$$\{\lambda_j\} = \text{eig}(A)$$

$$|\lambda_j| < 1$$

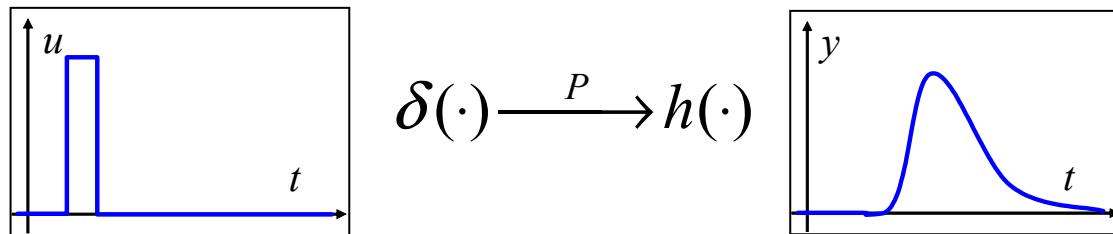


Example:

```
% Take A, B, C  
% from the R-W head example  
>> eig(A)  
>> ans =  
    1.0000  
    0.9980  
  
>>  
>> K = 10  
>> Ak = A - K*B*C;  
>> eig(Ak)  
>> ans =  
    0.9990  
    0.9990  
  
>>  
>> N = 2000;  
>> x(:,1) = [1; 0];  
>> for t=2:N,  
>>     x(:,t) = Ak*x(:,t-1);  
>> end  
>>  
>> plot(1:N,x(2,:))
```

Impulse response

- Response to an input impulse



- Sampled time: $t = 1, 2, \dots$
- Control history = linear combination of the impulses \Rightarrow system response = linear combination of the impulse responses

$$u(t) = \sum_{k=0}^{\infty} \delta(t - k)u(k)$$

$$y(t) = \sum_{k=0}^{\infty} h(t - k)u(k) = (h * u)(t)$$

Convolution representation of a sampled-time system

- Convolution

$$y(t) = \sum_{k=-\infty}^t h(t-k)u(k)$$

signal
processing $y = h * u$
notation

- Impulse response

$$u(t) = \delta(t) \quad \Rightarrow \quad y(t) = h(t)$$

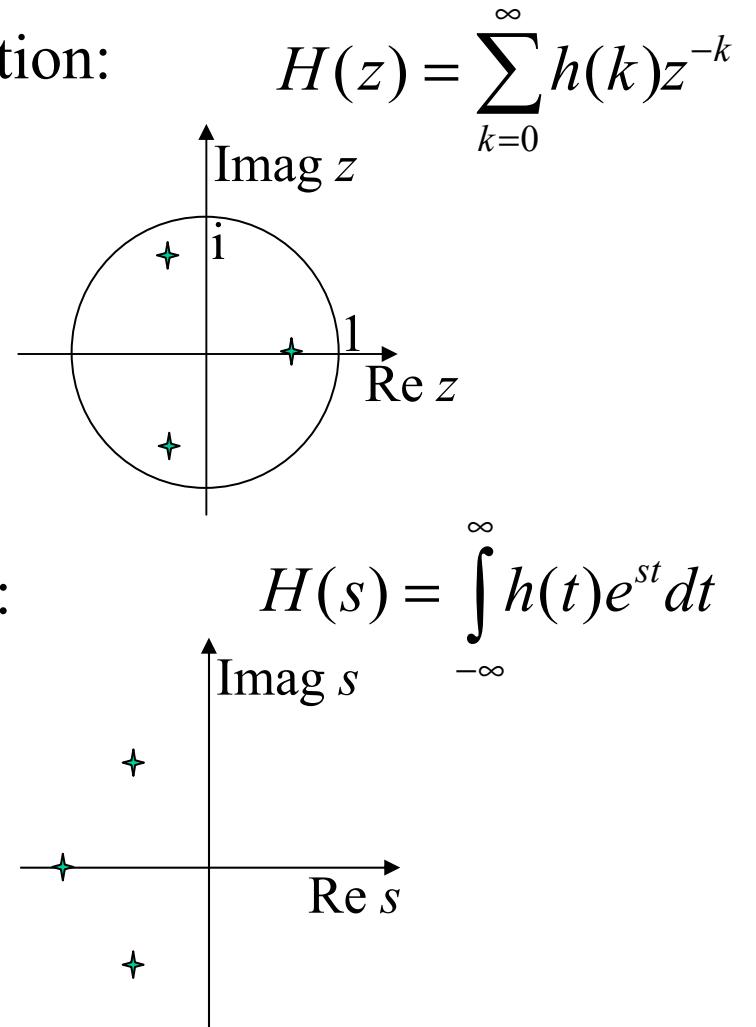
- Step response: $u = 1$ for $t > 0$

$$g(t) = \sum_{k=0}^t h(t-k) = \sum_{j=0}^t h(j) \quad h(t) = g(t) - g(t-1)$$

Matlab commands: `g = cumsum(h);` `h = diff(g);`

z -transform vs. Laplace transform

- Discrete (z -transform) transfer function:
 - function of complex variable z
 - $z \rightarrow$ forward shift operator
 - analytical outside the circle $|z| \geq r$
 - all poles are inside the circle
 - for a stable system $r \leq 1$
- Laplace transform transfer function:
 - function of complex variable s
 - $s \rightarrow$ differentiation operator
 - analytical in a half plane $\text{Re } s \leq a$
 - for a stable system $a \leq 1$

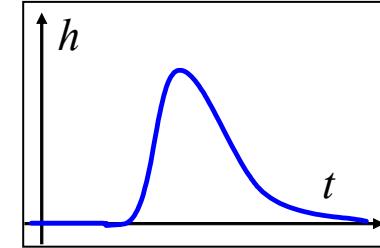


Sampled time vs. continuous time

- Continuous time analysis (digital implementation of a continuous time controller)
 - Tustin's method = trapezoidal rule of integration for $H(s) = \frac{1}{s}$
$$H(s) \rightarrow H_s(z) = H\left(s = \frac{2}{T} \cdot \frac{1-z^{-1}}{1+z^{-1}}\right)$$
 - Matched Zero Pole: map each zero and a pole in accordance with $s = e^{zT}$
- Sampled time analysis (Sampling of continuous signals and system)
- Systems analysis is often performed continuous time - this is where the controlled plant is.

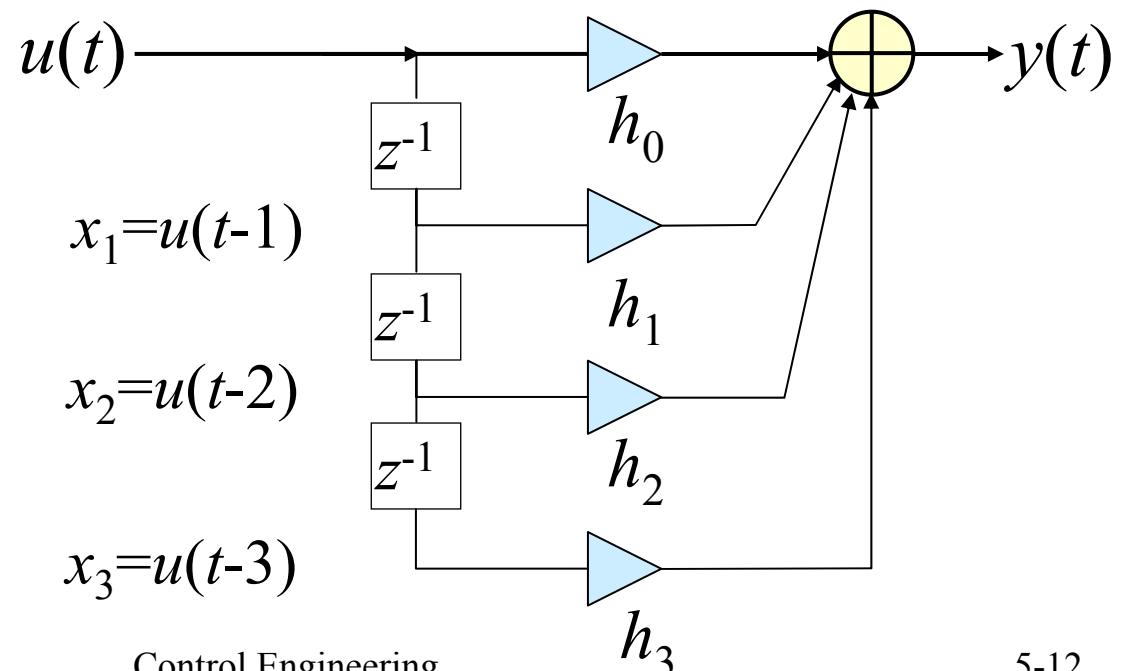
FIR model

$$y(t) = \sum_{k=0}^N h_{FIR}(t-k)u(k) = (h_{FIR} * u)(t)$$



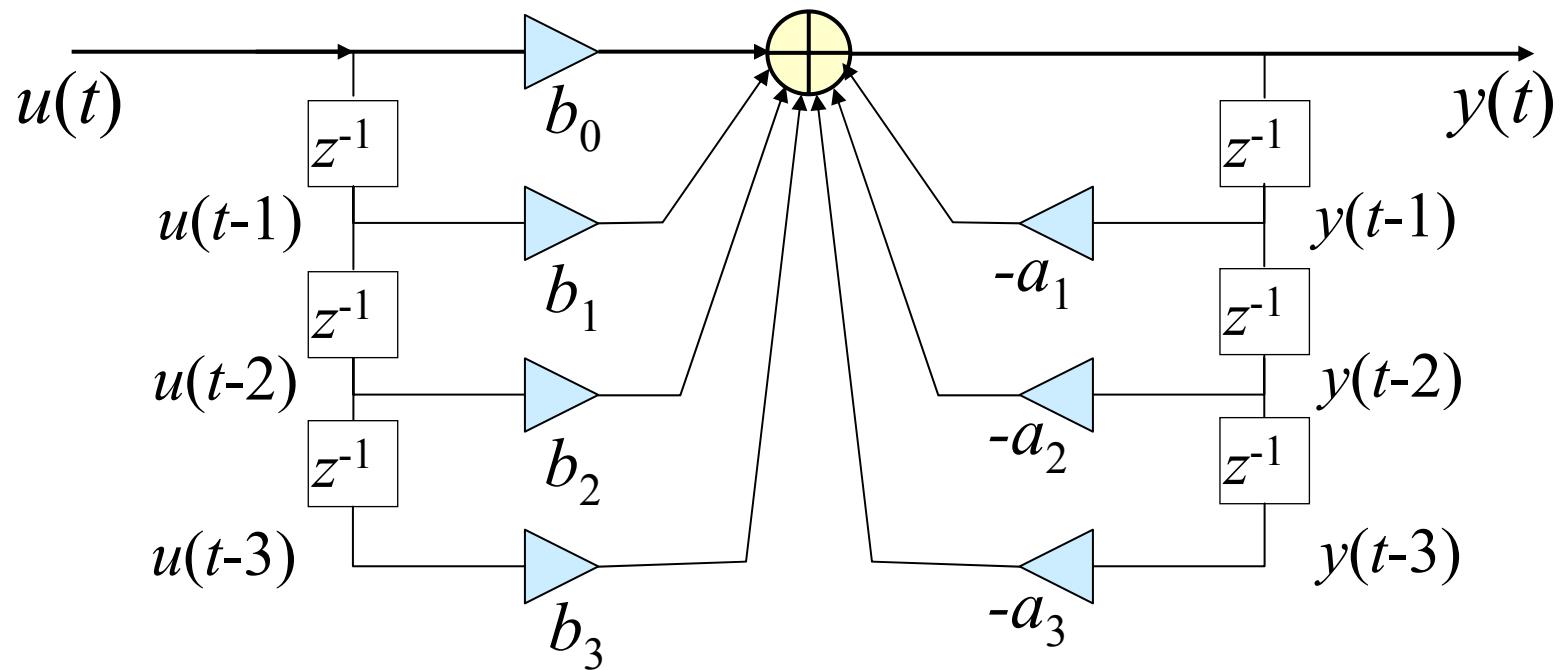
- FIR = Finite Impulse Response
- Cut off the trailing part of the impulse response to obtain FIR
- FIR filter state x is the shift register content

$x(t+1) = Ax(t) + Bu(t)$
$y(t) = Cx(t)$



IIR model

- IIR model: $y(t) = -\sum_{k=1}^{n_a} a_k y(t-k) + \sum_{k=0}^{n_b} b_k u(t-k)$
- Filter states: $y(t-1), \dots, y(t-n_a), u(t-1), \dots, u(t-n_b)$



IIR model

- Matlab implementation of an IIR model: **filter**
- Transfer function realization: unit delay operator z^{-1}

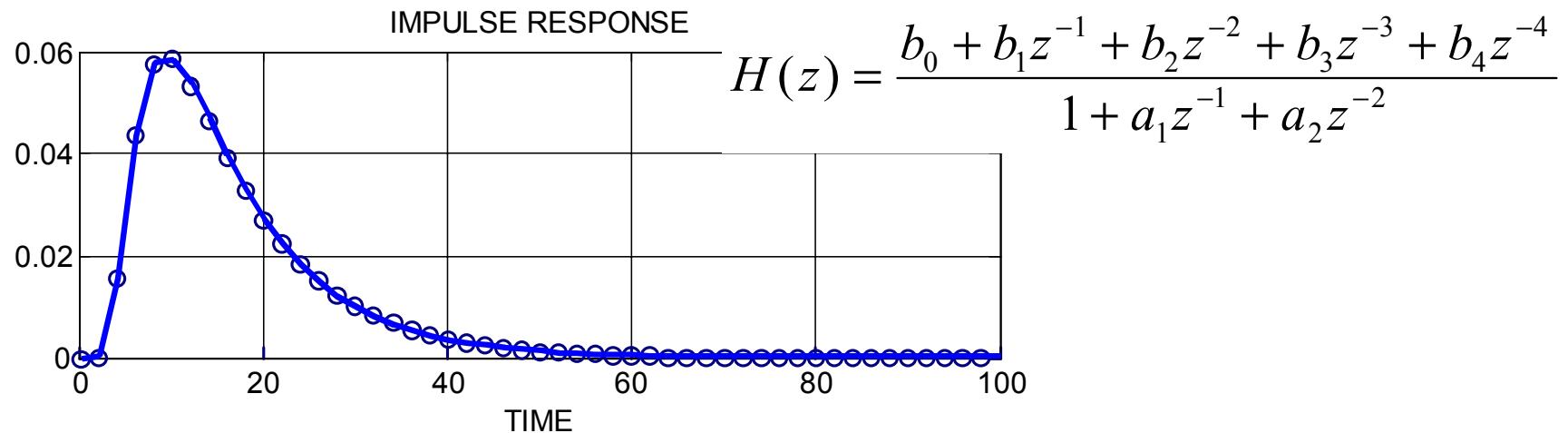
$$y(t) = H(z)u(t)$$

$$\begin{aligned} H(z) &= \frac{B(z)}{A(z)} = \frac{b_0 z^N + b_1 z^{N-1} + \dots + b_N}{z^N + a_1 z^{N-1} + \dots + a_N} && \text{Control convention} \\ &= \frac{b_0 + b_1 z^{-1} + \dots + b_N z^{-N}}{1 + a_1 z^{-1} + \dots + a_N z^{-N}} && \text{Matlab } \texttt{tf}, \text{ } \texttt{step} \text{ etc} \end{aligned}$$
$$\underbrace{(1 + a_1 z^{-1} + \dots + a_N z^{-N})}_{A(z)} y(t) = \underbrace{(b_0 + b_1 z^{-1} + \dots + b_N z^{-N})}_{B(z)} u(t)$$
$$\text{Signal processing convention}$$
$$\text{Matlab } \texttt{filter} \text{ etc}$$

- FIR model is a special case of an IIR with $A(z)=1$ (or z^N)

IIR approximation example

- Low order IIR approximation of impulse response:
(prony in Matlab Signal Processing Toolbox)
- Fewer parameters than a FIR model
- Example: sideways heat transfer
 - impulse response $h(t)$
 - approximation with IIR filter $a = [a_1 \ a_2]$, $b=[b_0 \ b_1 \ b_2 \ b_3 \ b_4]$



Linear state space model

- LTI state space model

$$\boxed{\begin{aligned}x(t+1) &= Ax(t) + Bu(t) \\y(t) &= Cx(t) + Du(t)\end{aligned}}$$

- Unit delay operator z^{-1} : $z^{-1}x(t) = x(t-1)$
- Transfer function of an LTI model
 - defines an IIR representation

$$y = [(Iz - A)^{-1}B + D] \cdot u$$

$$H(z) = C(Iz - A)^{-1}B + D$$

- Stability: the poles are inside the unit circle

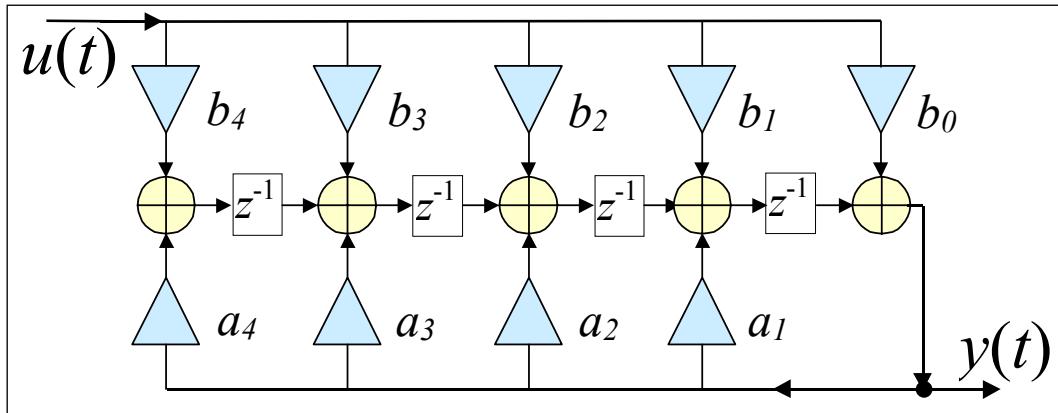
Stability analysis

- Transfer function poles tell you everything about stability
- Model-based analysis for a simple feedback example:

$$\begin{aligned}y &= H(z)u \\ u &= -K(y - y_d)\end{aligned}\quad \longrightarrow\quad y = \frac{H(z)K}{1 + H(z)K} y_d = L(z)y_d$$

- If $H(z)$ is a rational transfer function describing an IIR model
- Then $L(z)$ also is a rational transfer function describing an IIR model

State space realization of IIR filter



$$y(t) = H(z)u(t)$$

$$H(z) = \frac{B(z)}{A(z)} = \frac{b_0 + b_1 z^{-1} + \dots + b_N z^{-N}}{1 + a_1 z^{-1} + \dots + a_N z^{-N}}$$

$$\begin{bmatrix} x_1(t+1) \\ x_2(t+1) \\ x_3(t+1) \\ x_4(t+1) \end{bmatrix} = \begin{bmatrix} -a_1 & -a_2 & -a_3 & -a_3 \\ 1 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 1 & 0 \end{bmatrix} \cdot \begin{bmatrix} x_1(t) \\ x_2(t) \\ x_3(t) \\ x_4(t) \end{bmatrix} + \begin{bmatrix} 1 \\ 0 \\ 0 \\ 0 \end{bmatrix} u(t)$$

$$y(t) = [b_1 - a_1 b_0 \quad b_2 - a_2 b_0 \quad b_3 - a_3 b_0 \quad b_4 - a_4 b_0] \cdot \begin{bmatrix} x_1(t) \\ x_2(t) \\ x_3(t) \\ x_4(t) \end{bmatrix} + b_0 u(t)$$

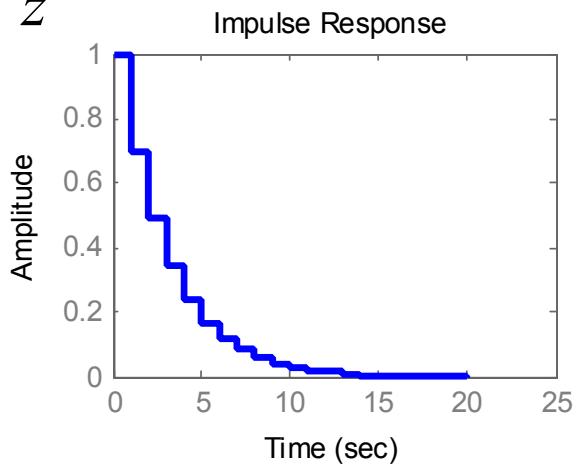
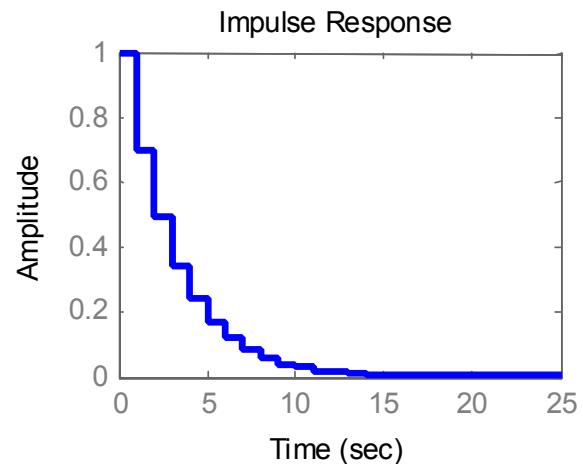
Poles and Zeros \leftrightarrow System

- ...not quite so!
- Example:

$$y = H(z)u = \frac{z}{z - 0.7}$$

- FIR model - truncated IIR

$$y = H_{FIR}(z)u = \frac{z^{19} + 0.7z^{18} + 0.49z^{17} + \dots + 0.001628 z + 0.00114}{z^{19}}$$



IIR/FIR example - cont'd

- Feedback control:

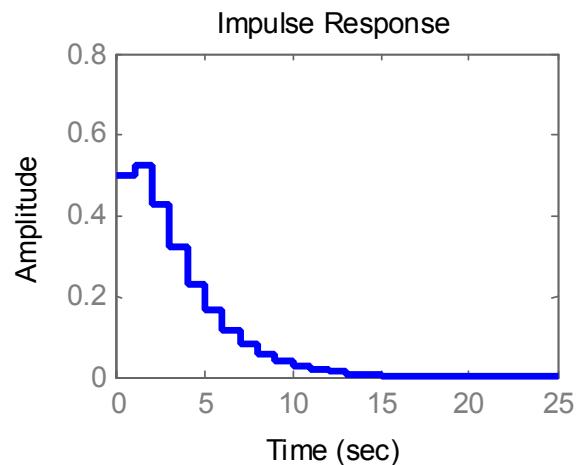
$$y = H(z)u = \frac{z}{z - 0.7}$$

$$u = -K(y - y_d) = -(y - y_d)$$

- Closed loop:

$$y = \frac{H(z)}{1 + H(z)}u = L(z)u$$

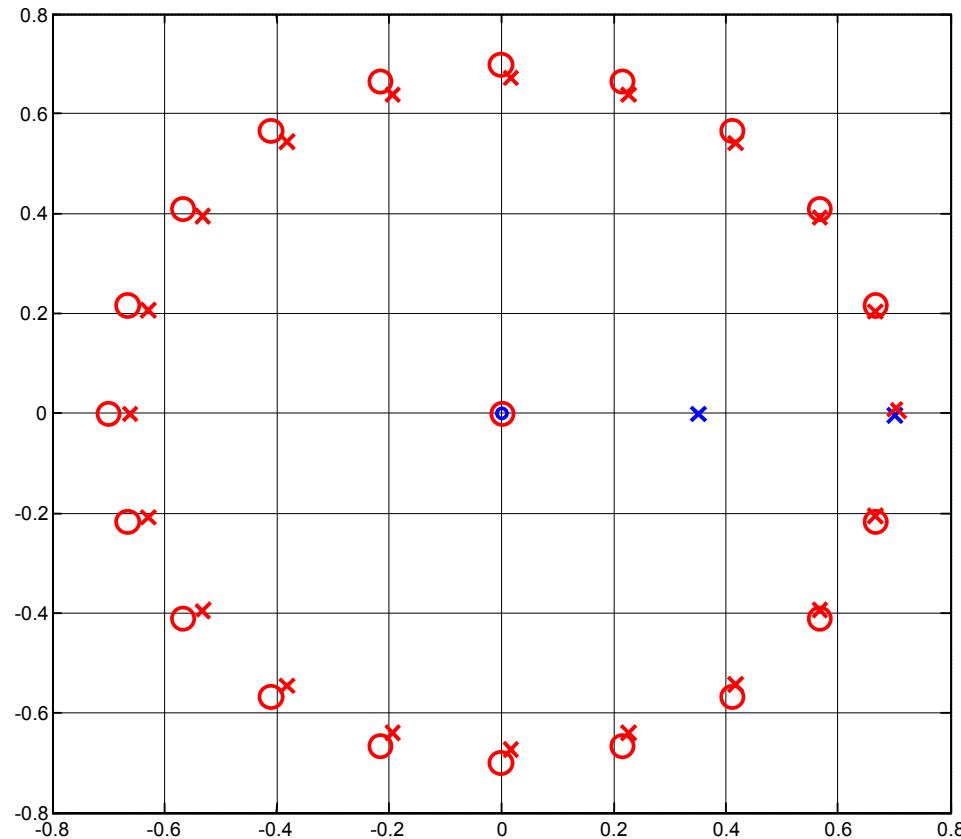
$$y = \frac{H_{FIR}(z)}{1 + H_{FIR}(z)}u = L_{FIR}(z)u$$



IIR/FIR example - cont'd

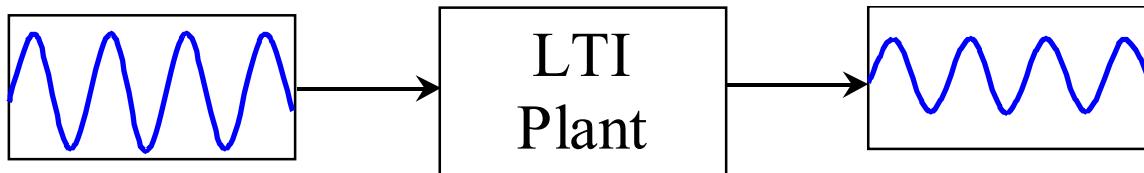
Poles and zeros

- **Blue:** Loop with IIR model poles **x** and zeros **o**
- **Red:** Loop with FIR model poles **x** and zeros **o**



Frequency domain description

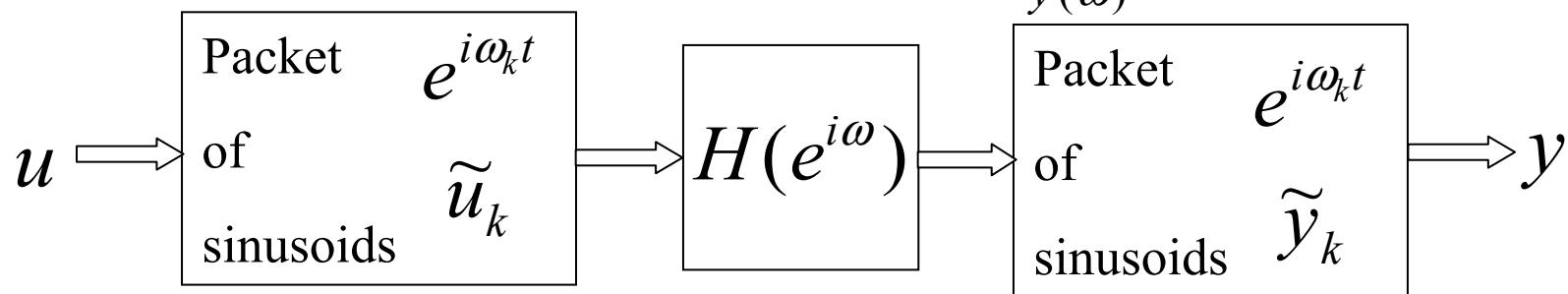
- Sinusoids are eigenfunctions of an LTI system: $y = H(z)u$



$$ze^{i\omega t} = e^{i\omega(t+1)} = e^{i\omega} e^{i\omega t} \quad z \rightarrow e^{i\omega}$$

- Frequency domain analysis \leftrightarrow system diagonalization

$$u = \sum \tilde{u}_k e^{i\omega_k t} \Rightarrow y = \sum \underbrace{H(e^{i\omega_k}) \tilde{u}_k e^{i\omega_k t}}_{\tilde{y}(\omega)}$$



Frequency domain description

- Bode plots:

$$u = e^{i\omega t}$$

$$y = H(e^{i\omega})e^{i\omega t}$$

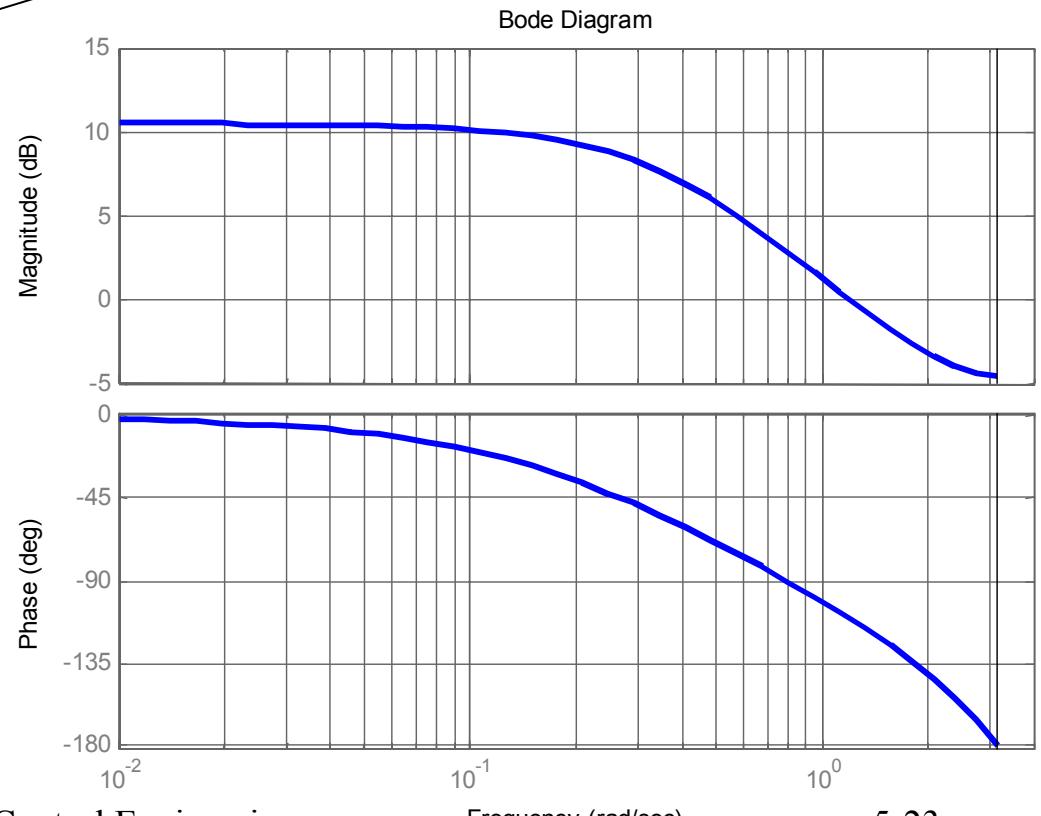
- Example:

$$H(z) = \frac{1}{z - 0.7}$$

- $|H|$ is often measured in dB

$$M(\omega) = |H(e^{i\omega})|$$

$$\varphi(\omega) = \arg H(e^{i\omega})$$



Fourier transform for sampled signals

$$\tilde{x}(\omega) = \sum_{t=-\infty}^{\infty} x(t)e^{i\omega t}$$

$$x(t) = \frac{1}{2\pi} \int_0^{2\pi} \tilde{x}(\omega)e^{-i\omega t} d\omega$$

- Fourier transform of a series $[-\infty : 1 : \infty] \rightarrow [0, 2\pi]$
- Inverse Fourier transform $[0, 2\pi] \rightarrow [-\infty : 1 : \infty]$

- If $x(t)$ is a smoothly varying signal, the sum approximates the integral for continuous FT
- $\tilde{x}(\omega)$ approximates the continuous FT up to the Nyquist frequency of $\omega = \pi$
- If sampling frequency is other than unity, need to scale

Discrete Fourier Transform = DFT

DFT is computed by Matlab **FFT**

$$\tilde{x}(\omega_k) = \sum_{t=1}^N x(t)e^{i\omega_k t}, \quad \omega_k = \frac{2\pi}{N}k \quad \bullet \quad \text{DFT}$$

f=FFT(x)

$$[0:1:N] \rightarrow [0:(2\pi/N):2\pi]$$
$$x(t) = \frac{1}{N} \sum_{k=0}^{N-1} \tilde{x}(\omega_k) e^{-i\omega_k t} \quad \bullet \quad \text{Inverse DFT}$$

x=iFFT(f)

$$[0:(2\pi/N):2\pi] \rightarrow [0:1:N]$$

- DFT = FT of a sequence: ..., 0, $x(1)$, $x(2)$, ..., $x(N)$, 0, 0, ...
- The sum in Inverse DFT approximates the infinite sequence inverse FT up to the ‘Nyquist time’ of $N/2$

Sampled-time LTI models - recap

- Linear system can be described by impulse response
- Linear system can be described by frequency response = Fourier transform of the impulse response
- FIR, IIR, State-space models can be used to obtain close approximations of sampled-time linear system
- A pattern of poles and zeros can be very different for a small change in an input-output model.
- Impulse response, step response, and frequency response do not change much for small model changes

Sampled time I control

- Step to step update:

$$y(t) = g \cdot u(t) + d(t)$$

$$u(t) = u(t-1) + v(t-1)$$

$$v(t) = k_I [y(t) - y_d]$$

*sampled time
integrator*

- Closed-loop dynamics

$$\begin{aligned} y &= g \cdot u + d \\ u &= \frac{k_I}{z-1} [y - y_d] \end{aligned} \quad \longrightarrow \quad y = \frac{gk_I}{z-1+gk_I} y_d + \frac{z-1}{z-1+gk_I} d$$

- Deadbeat control: $gk_I = 1 \quad \longrightarrow \quad y = z^{-1} y_d + (1 - z^{-1}) d$

Run-to-run (R2R) control

- Main APC (Advanced Process Control) approach in semiconductor processes
- Modification of a product recipe between tool "runs"



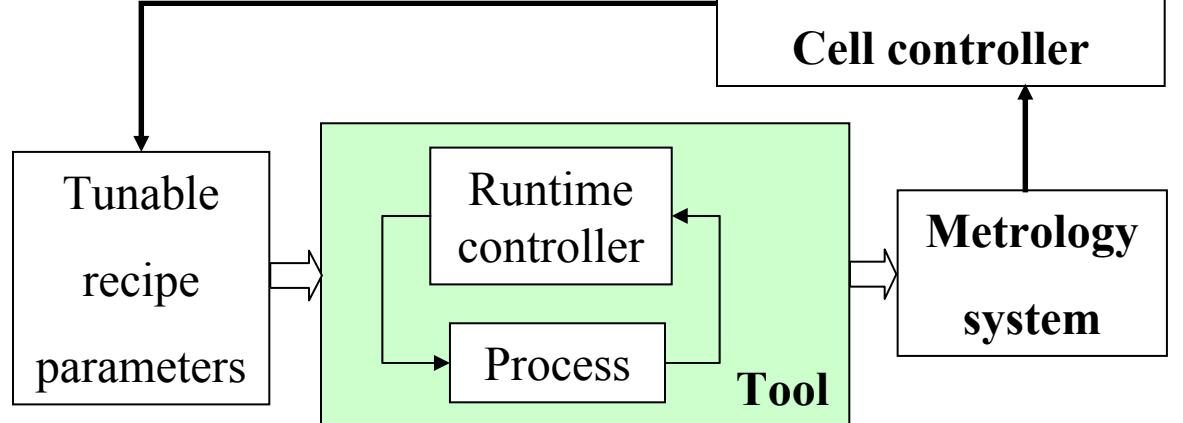
- Processes:

- vapor phase epitaxy
- lithography
- chemical mechanical planarization (CMP)
- plasma etch

$$y(t) = g \cdot u(t) + d(t)$$

$$u(t) = u(t-1) - k_I [y(t) - y_d]$$

Run-to-run control
Cell controller



PI control

- P Control + Integrator for cancelling steady state error

$$e = y - y_d$$

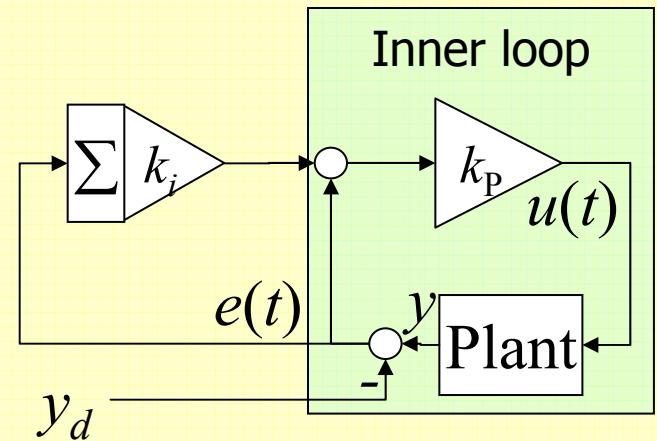
$$v(t+1) = v(t) + e(t)$$

$$u(t) = -k_I v(t) - k_P e(t)$$

- Velocity form of the controller

$$u(t) = u(t-1) - k_I e(t) - k_P [e(t) - e(t-1)]$$

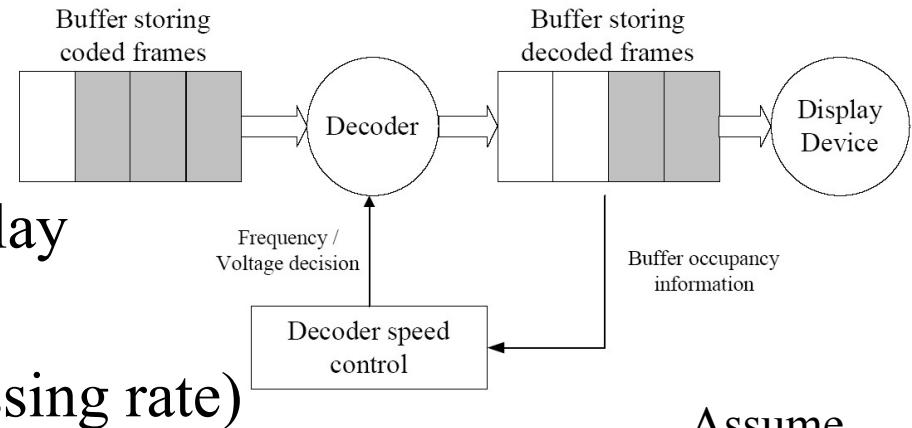
Cascade loop interpretation:



$$k_I = k_i \cdot k_P$$

QoS Control Example

- QoS control for video server
 - QoS = Quality of Service
 - Need to maintain constant delay
 - for audio synchronization etc
 - Control codec quality (processing rate)
 - Regulate buffer queue
 - Model:
- Assume $T = 1$
- | | |
|--------|----------------------------------|
| Rate | $r(t + 1) = u(t)$ |
| Buffer | $b(t + 1) = b(t) - Tr(t) + w(t)$ |



$$x(k+1) = \underbrace{\begin{bmatrix} 0 & 0 \\ -1 & 1 \end{bmatrix}}_A \cdot x(k) + \underbrace{\begin{bmatrix} -1 \\ 0 \end{bmatrix}}_B \cdot u(k) + \underbrace{\begin{bmatrix} 0 \\ 1 \end{bmatrix}}_F \cdot w(k)$$

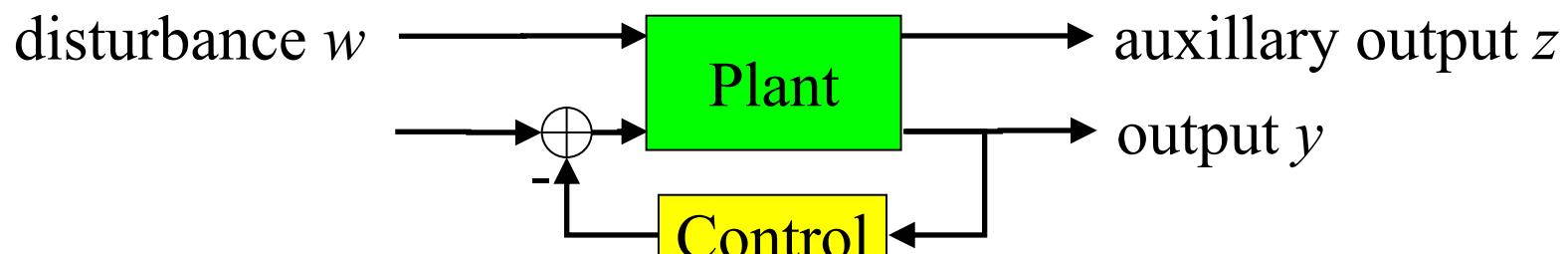
$$y(k) = \underbrace{\begin{bmatrix} 0 & 1 \end{bmatrix}}_C \cdot x(k)$$

QoS Control Example, cont'd

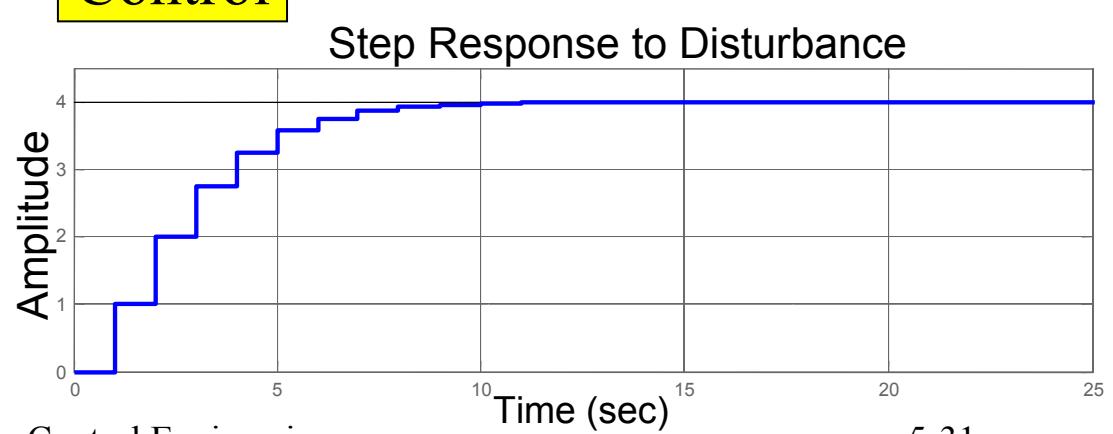
- Dominant integrator dynamics, use P control

$$x(k+1) = Ax(k) + Bu(k) + Fw(k) \quad u(k) = -k_P(y(k) - y_d)$$

$$y(k) = Cx(k)$$



Matlab command:
`S=feedback(P,C,iI,i0);`
Use `tf` to convert model



QoS Control Example, cont'd

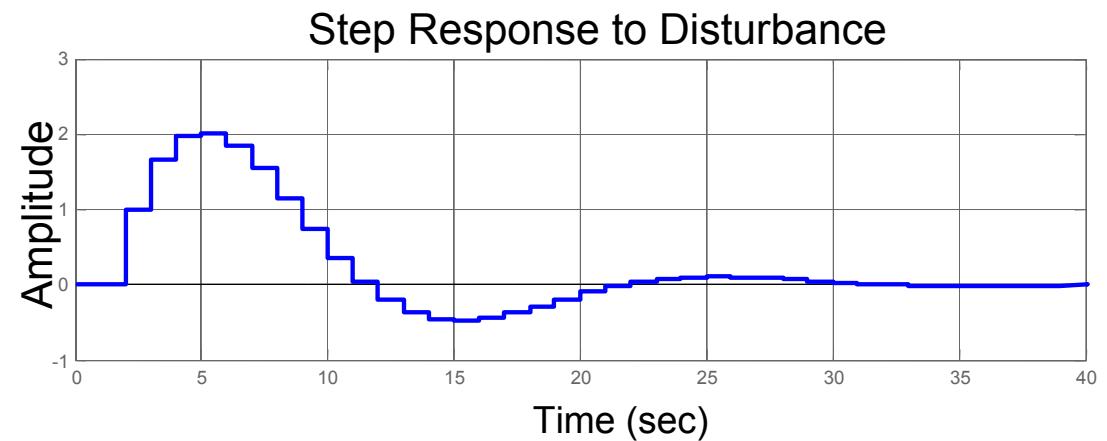
- P control provides poor disturbance rejection
- Use PI control

$$e(k) = y(k) - y_d$$

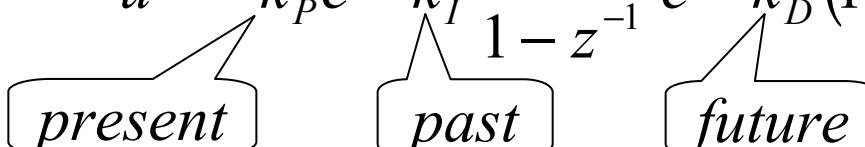
$$u(k) = u(k-1) - k_I e(k) - k_P [e(k) - e(k-1)]$$

- PI has better disturbance rejection

$$u = - \left[k_P + \frac{k_I z}{z-1} \right] \cdot e$$



PID Control

- PID: three-term control $e = y - y_d$
 $u = -k_P e - k_I \int e \cdot dt - k_D \dot{e}$
- Sampled-time PID $u = -k_P e - k_I \frac{1}{1 - z^{-1}} e - k_D (1 - z^{-1}) \cdot e$


- PID controller in velocity form $\Delta u = -k_D \Delta^2 e - k_P \Delta e - k_I e$
– bumpless transfer between
manual and automatic $\Delta = 1 - z^{-1}$

$$u(t) = u(t-1) - k_I e(t) - k_P [e(t) - e(t-1)] - k_D [e(t) - 2e(t-1) + e(t-2)]$$

PID Controller Tuning

- Tune continuous-time PID controller, e.g. by Ziegler-Nichols rule, and set up the sampled time PID to approximate the continuous-time PID
- Cascaded loop design (continuous time structure)
 - Design P
 - Cascade I, retune P
 - Add D, retune PI
- Optimize the performance parameters by repeated simulation runs – search through the {P, I, D} space
- Loopshaping – Lectures 7-8
- Advanced control design – formal specs, other courses

Industrial PID Controller

- A box, not an algorithm
- Auto-tuning functionality:
 - pre-tune
 - self-tune
- Manual/cascade mode switch
- Bumpless transfer between different modes, setpoint ramp
- Loop alarms
- Networked or serial port connection



Plant Type

- Constant gain - I control
- Integrator - P control
- First order system - PI control
- Double integrator or second order system - PD control
- Generic response with delay - PID control